



Chemical Thermodynamics

Chem 211: Lecture 6

Applications of 1st law
of Thermodynamics

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Outline

- Heat capacity
- c_p/c_v Relationship for ideal gases
- Adiabatic index
- Effect of T on heat of reaction
- Kirschoff's Law
- Adiabatic expansion
- Joule experiment
- Joule-Thomson effect
- Inversion Temperature

Heat Capacity, C

is the amount of heat necessary to raise the temperature of a certain substance (or system) one degree (Extensive property).

$$C = \frac{dq}{dT}$$

Heat Capacity at constant P (C_P)

is the amount of heat necessary to raise the temperature of a certain substance (or system) one degree at a constant pressure.

$$C_P = \frac{dq_P}{dT}$$

$$dq_P = dH = dU + PdV$$

$$C_P = \left(\frac{dq}{dT} \right)_P = \left(\frac{dH}{dT} \right)_P = \left(\frac{dU}{dT} \right)_P + P \left(\frac{dV}{dT} \right)_P$$

Heat Capacity at constant V (C_V)

is the amount of heat necessary to raise the temperature of a certain substance (or system) one degree at a constant volume.

$$C_V = \frac{dq_V}{dT}$$

$$dq_V = dU \quad \rightarrow$$

$$C_V = \left(\frac{dq}{dT} \right)_V = \left(\frac{dU}{dT} \right)_V$$

Molar Heat Capacity, c

is the amount of heat necessary to raise the temperature of one mole of a certain substance (or system) one degree (intensive property)

$$c = \frac{dq}{ndT}$$

n: no. of moles

Molar heat capacity at constant P (c_p)

is the amount of **heat** necessary to **raise** the temperature of **one** mole of a certain substance (or system) **one** degree at constant pressure.

Molar heat capacity at constant V (c_v)

is the amount of **heat** necessary to **raise** the temperature of **one mole** of a certain substance (or system) **one degree at constant volume**.

Specific heat capacity (S)

is the amount of heat necessary to **raise** the temperature of **one gram** of a certain substance (or system) **one** degree (intensive property)

$$S = \frac{dq}{mdT}$$

m : mass (g)

Exercise

A 2.50 kg piece of copper metal is heated from 25°C to 225°C. How much heat, in kJ, is absorbed by the copper? The specific heat of copper is 0.384 J/g °C.

Answer

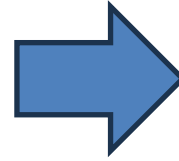
$$s = \frac{dq}{m dT} = \frac{q}{m \Delta T}$$

$$q = ms\Delta T = (2.5 \text{ kg}) \left(\frac{0.384 \text{ J}}{\text{g}^\circ\text{C}} \right) (200^\circ\text{C})$$
$$= 192 \text{ kJ}$$

c_p/c_v Relationship for ideal gases

$$H = U + PV$$

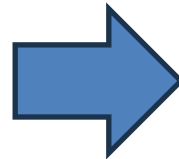
$$dH = dU + PdV$$



$$\frac{dH}{dT} = \frac{dU}{dT} + \frac{PdV}{dT}$$

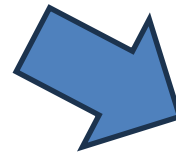
For one mole of an ideal gas, $n=1$

$$PV = RT$$



$$\frac{PdV}{dT} = R$$

$$\frac{dH}{dT} = \frac{dU}{dT} + R$$



$$c_p = c_v + R$$

$$\text{kJ mol}^{-1} \text{K}^{-1}$$

According to kinetic molecular theory of gases

The **thermal energy** of a mono-atomic gas consists solely of **translational energy** of motion of the atoms in the space and equal to $3RT/2$.

$$U = \frac{3}{2}RT$$

$$\left(\frac{dU}{dT}\right)_V = c_V = \frac{3}{2}R$$

$$c_P = c_V + R$$

$$c_P = c_V + R = \frac{3}{2}R + R = \frac{5}{2}R$$

Adiabatic index, γ

In thermal physics and thermodynamics, the heat capacity ratio or adiabatic index or ratio of specific heats or Poisson constant, is the ratio of the heat capacity at constant pressure (c_p) to heat capacity at constant volume (c_v).

$$\gamma = \frac{c_p}{c_v}$$

$$\gamma = \frac{c_p}{c_v} = \frac{c_v + R}{c_v} = \frac{\frac{3}{2}R + R}{\frac{3}{2}R} = \frac{\frac{5}{2}R}{\frac{3}{2}R} = \frac{5}{3} = 1.67$$

For poly-atomic gases  $U > \frac{3}{2}RT$

due to contributions from rotational and vibrational motions

Therefore,

$$\gamma = \frac{C_P}{C_V} < 1.67$$

Generally,

$$\gamma = \frac{C_P}{C_V} = \frac{C_V + R}{C_V} = 1 + \frac{R}{C_V}$$

$C_V \uparrow \rightarrow \gamma \downarrow$

Effect of T on heat of reaction

- The **heat** of reaction (**physical or chemical change**) depends **on T**.
- **For any system**, on going from a state A to state B,

$$\Delta H = H_B - H_A$$

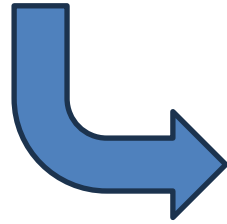
Take a differentiation with respect to T at constant P

$$\left(\frac{d\Delta H}{dT}\right)_P = \left(\frac{dH_B}{dT}\right)_P - \left(\frac{dH_A}{dT}\right)_P = c_{P,B} - c_{P,A} = \Delta c_P$$

Kirschhoff's equation

$$d\Delta H = \Delta c_P dT$$

$$d\Delta H = \Delta c_p dT$$



$$\int_{\Delta H_1}^{\Delta H_2} d\Delta H = \int_{T_1}^{T_2} \Delta c_p dT$$

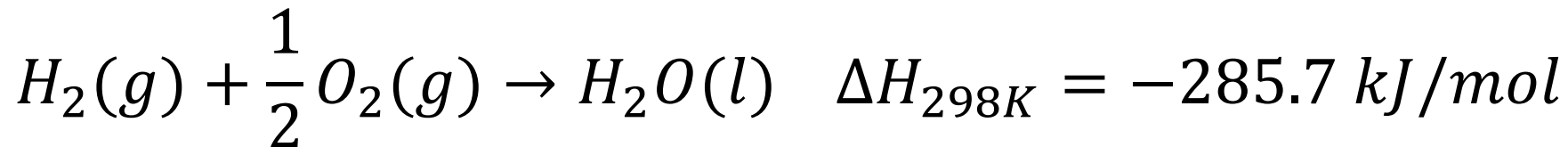
ΔH_1 and ΔH_2 : heats of reaction at T_1 and T_2 , respectively.

- Assuming ΔC_p is **independent** of T in the assigned domain (between T_1 and T_2) therefore,

$$\Delta H_2 - \Delta H_1 = q_P = \Delta c_p (T_2 - T_1)$$

Exercise

✚ The heat of formation of liquid water at 25°C is -285.7 kJ/mol . The mean molar heat capacities of $\text{H}_2(\text{g})$, $\text{O}_2(\text{g})$, and $\text{H}_2\text{O}(\text{l})$ are 28.8, 29.1, and 75.3 $\text{Jmol}^{-1}\text{K}^{-1}$. Calculate the heat of formation of water at 100 °C.

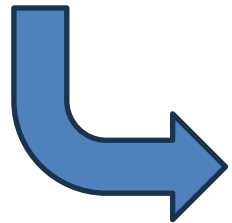


Answer

$$\Delta C_P = C_{P,\text{H}_2\text{O}} - C_{P,\text{H}_2} - \frac{1}{2} C_{P,\text{O}_2}$$

$$= 75.3 - 28.8 - \frac{1}{2}(29.1) =$$
$$31.95 \text{ Jmol}^{-1}\text{K}^{-1} = 0.032 \text{ kJ mol}^{-1}\text{K}^{-1} \text{ at } 25^\circ\text{C}$$

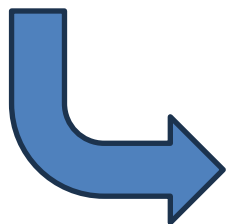
$$\int_{\Delta H_1}^{\Delta H_2} d\Delta H = \int_{T_1}^{T_2} \Delta c_p dT$$



$$\Delta H_2 - \Delta H_1 = q_P = \Delta c_p (T_2 - T_1)$$

$$\Delta H_{373K} - \Delta H_{298K} = 0.032(373 - 298)$$

$$\Delta H_{373K} - (-285.7 \text{ kJ/mol}) = 2.4$$



$$\Delta H_{373K} = -283.3 \text{ kJ/mol}$$

Hypothetical $\Delta H_{\text{reaction}}$ at 0K

- ✚ The integrated **Kirschhoff's** equation can be used to calculate the hypothetical heat of reaction at the absolute zero.

$$\Delta H_2 - \Delta H_1 = \int_{T_1}^{T_2} \Delta c_p dT$$

c_p is T 's dependent

$$\Delta c_p = a + bT + cT^2 + \dots \text{etc}$$

$$\Delta H_2 = \Delta H_1 + \int_{T_1}^{T_2} (a + bT + cT^2 + \dots) dT$$

$$\Delta H_2 = \Delta H_1 + \left(aT + \frac{bT^2}{2} + \frac{cT^3}{3} + \dots \right)$$

Exercise

✚ The heat of formation of ammonia at 25°C is -92.4 kJ/mol. The molar heat capacities of $N_2(g)$, $H_2(g)$, and ammonia at constant pressure are function of temperatures and given by the following equations in $J mol^{-1}K^{-1}$. Calculate the heat of formation of ammonia at 125 °C.

$$C_{P,N_2(g)} = 27.2 + 4.2(10^{-3}T)$$

$$C_{P,H_2(g)} = 27.2 + 3.8(10^{-3}T)$$

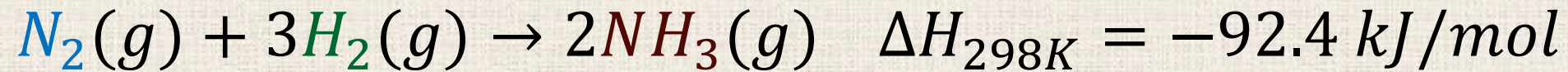
$$C_{P,NH_3(g)} = 33.6 + 2.9(10^{-3}T) + 2.1(10^{-5}T^2)$$

Answer



$$\text{for 2 moles } NH_3 = 2(-92.4) = 184.8 \text{ kJ}$$

$$\Delta C_P = 2C_{P,NH_3} - C_{P,N_2} - 3C_{P,H_2}$$



$$\begin{aligned} \Delta C_P &= 2 \left(33.6 + 2.9(10^{-3}T) + 2.1(10^{-5}T^2) \right) \\ &\quad - \left(27.2 + 4.2(10^{-3}T) \right) - 3 \left(27.2 + 3.8(10^{-3}T) \right) \\ &= -41.6 + 9.8(10^{-3}T) + 4.2(10^{-5}T^2) \text{ J mol}^{-1} \text{ K}^{-1} \end{aligned}$$

$$\int_{\Delta H_{1,298K}}^{\Delta H_{2,398K}} d\Delta H = \Delta H_{2,398K} - \Delta H_{1,298K} = \int_{298K}^{398K} \Delta C_P dT$$

$$\Delta H_{2,398K} - \Delta H_{1,298K} = \int_{298K}^{398K} \Delta c_p dT$$

$$= \int_{298K}^{398K} \left(-41.6 - 9.8(10^{-3}T) + 4.2(10^{-5}T^2) \right) dT$$

$$= -41.6(T_2 - T_1) - \frac{9.8 \times 10^{-3}(T_2^2 - T_1^2)}{2} + \frac{4.2 \times 10^{-5}(T_2^3 - T_1^3)}{3}$$

$$= -41.6(398 - 298) - \frac{9.8 \times 10^{-3}((398)^2 - (298)^2)}{2}$$

$$+ \frac{4.2 \times 10^{-5}((398)^3 - (298)^3)}{3}$$

$$\Delta H_{2,398K} - (-92400 \text{ J/mol}) = -4160 - 341 + 512$$

$$\Delta H_{2,398K} = 96389 \text{ J/mol} = 96.389 \text{ kJ/mol}$$

Homework

✚ Use the data provided in the last example to calculate the heat of formation of ammonia at 0K?

Rationalization of Kirschoff's Law

- ✚ It outlines the variation of a reaction's **enthalpy** with **temperature**.
- ✚ In general, **enthalpy** of any substance increases with **temperature**, which means both the products and the reactants' enthalpies increase.
- ✚ The overall enthalpy of the reaction will change if the increase in the enthalpy of products and reactants is different.

Δc_p is independent of T

$$\Delta H_2 = \Delta H_1 + \Delta c_p (T_2 - T_1)$$

Δc_p is +ve and $T_2 > T_1$, therefore, $\Delta H_2 > \Delta H_1$

Δc_p is T dependent

$$\Delta H_2 = \Delta H_1 + \int_{T_1}^{T_2} \Delta c_p dT$$

- ▶ The **change in enthalpy** is a function of the difference in temperature and heat capacities.
- ▶ It is proportional to the **product** of temperature change and change in heat capacities of products and reactants

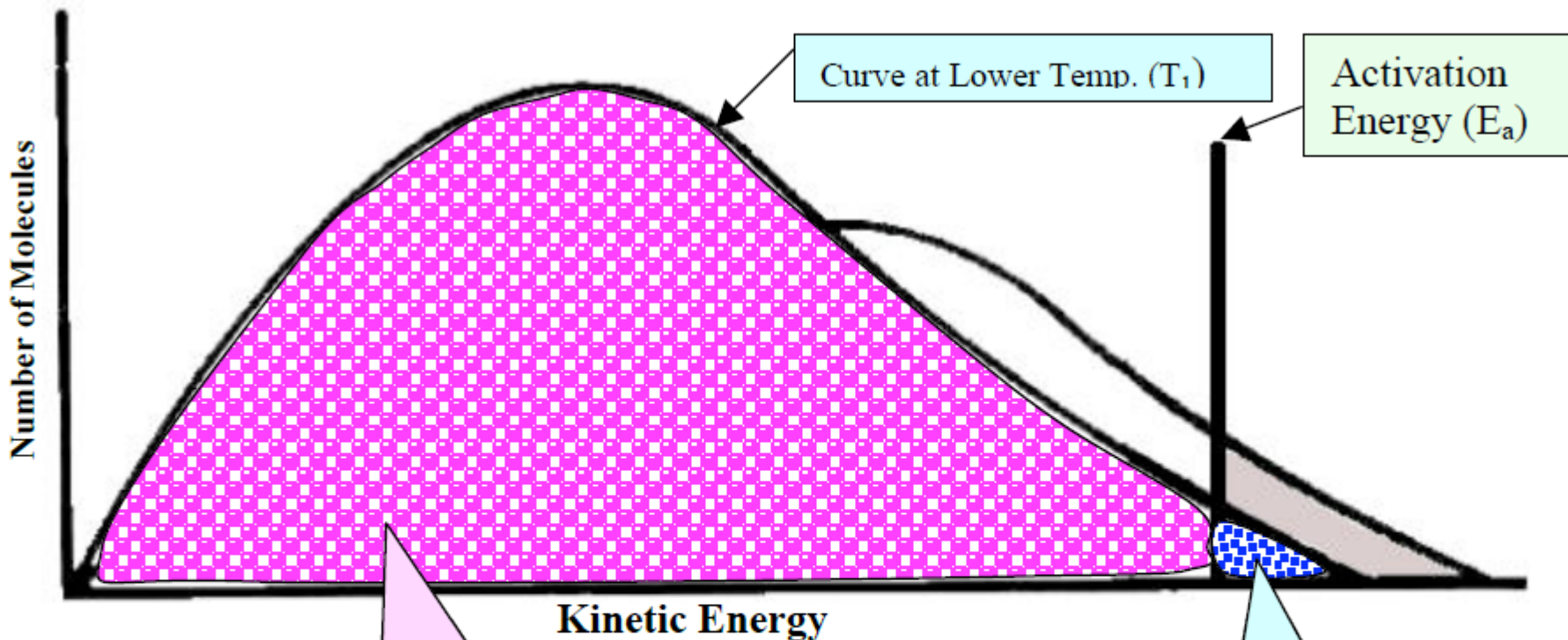
Consider a reaction



- proceeds at a given T_1 , which is necessary to overcome the activation energy (E_a) the reactants need to reach the transition state (state corresponding to the highest potential energy (PE) along this reaction coordinate) or sometimes called activated complex, AC.
- E_a (minimum energy required for a successful collision that produces AC by converting the KE into PE, bonds formation).
- E_a depends on nature of reactants (numbers & strengths of bonds in reactants) but do NOT depend on the change in T & concentration.

- # **AC** is a very **short-lived**, unstable combination of reactant atoms that exists before products are formed. It has different PE from that of reactants.
- # This change in PE is likely provided from the KE of the system which depends on T.
- # Once the **PE** of the reactants reaches this **TS**, the products will readily be formed.
- # If T_1 is **not sufficient** to move the reactants into this TS, the products will not form.
- # The **temperature** determines how many (or **what fraction** of the) molecules will have **energy** $> E_a$ (to make it over the barrier & have a successful collision)

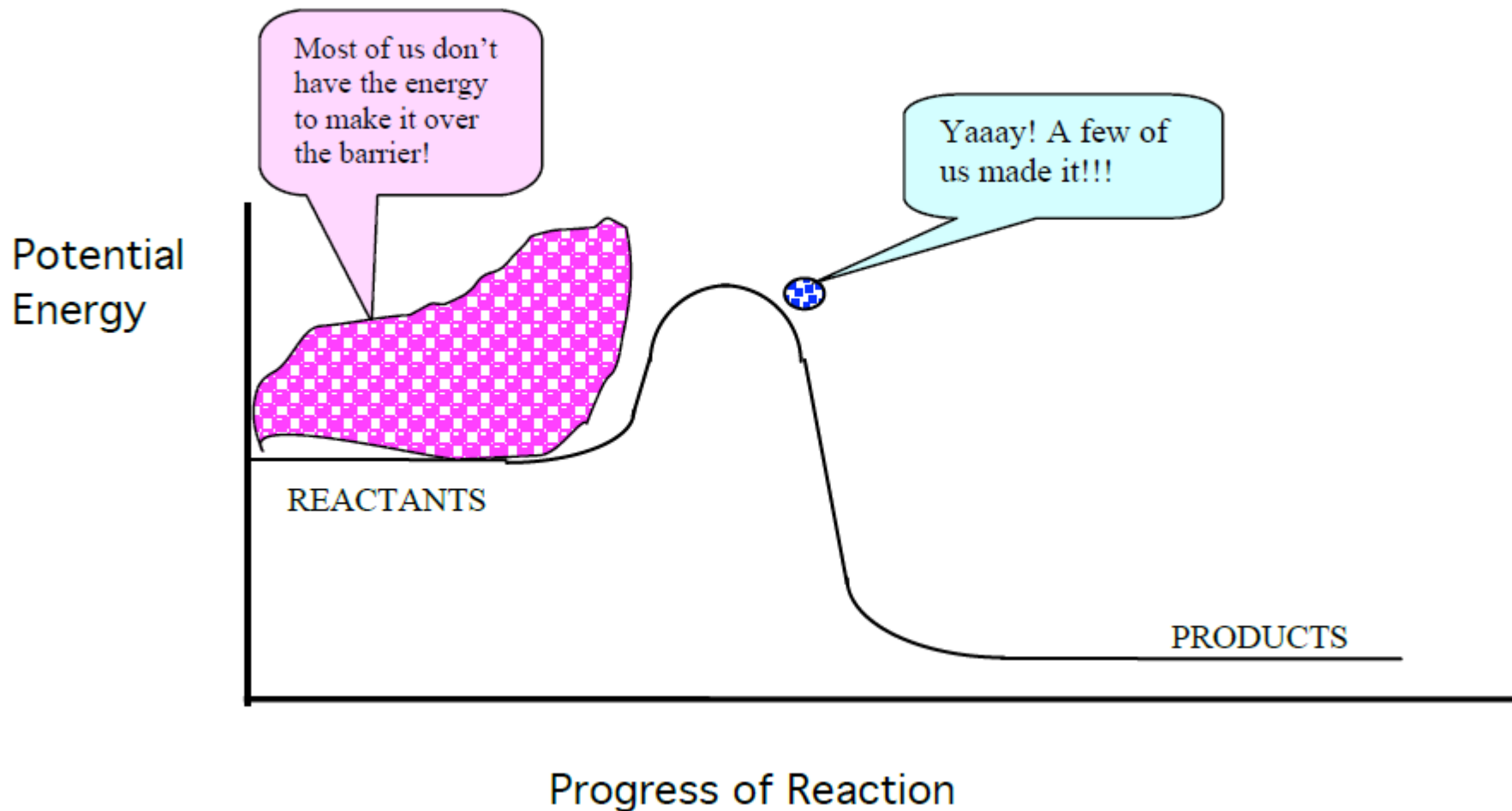
KE distributions at low T_1



At Temperature T_1 (lower temp), the molecules represented by this area do NOT have sufficient KE for a successful collision

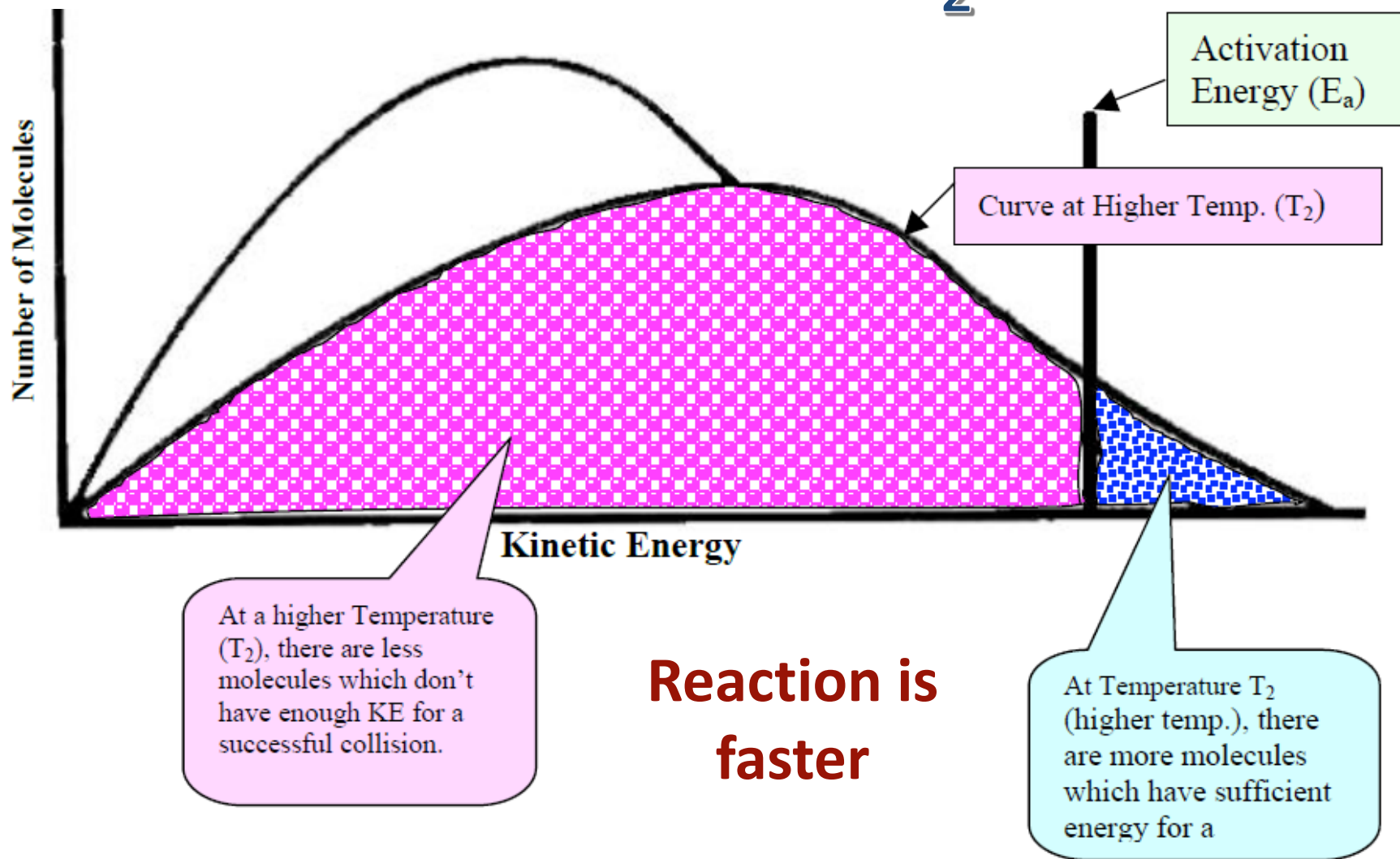
At Temperature T_1 (lower temp.), only these molecules have sufficient energy for a successful collision

KE distributions at low T_1



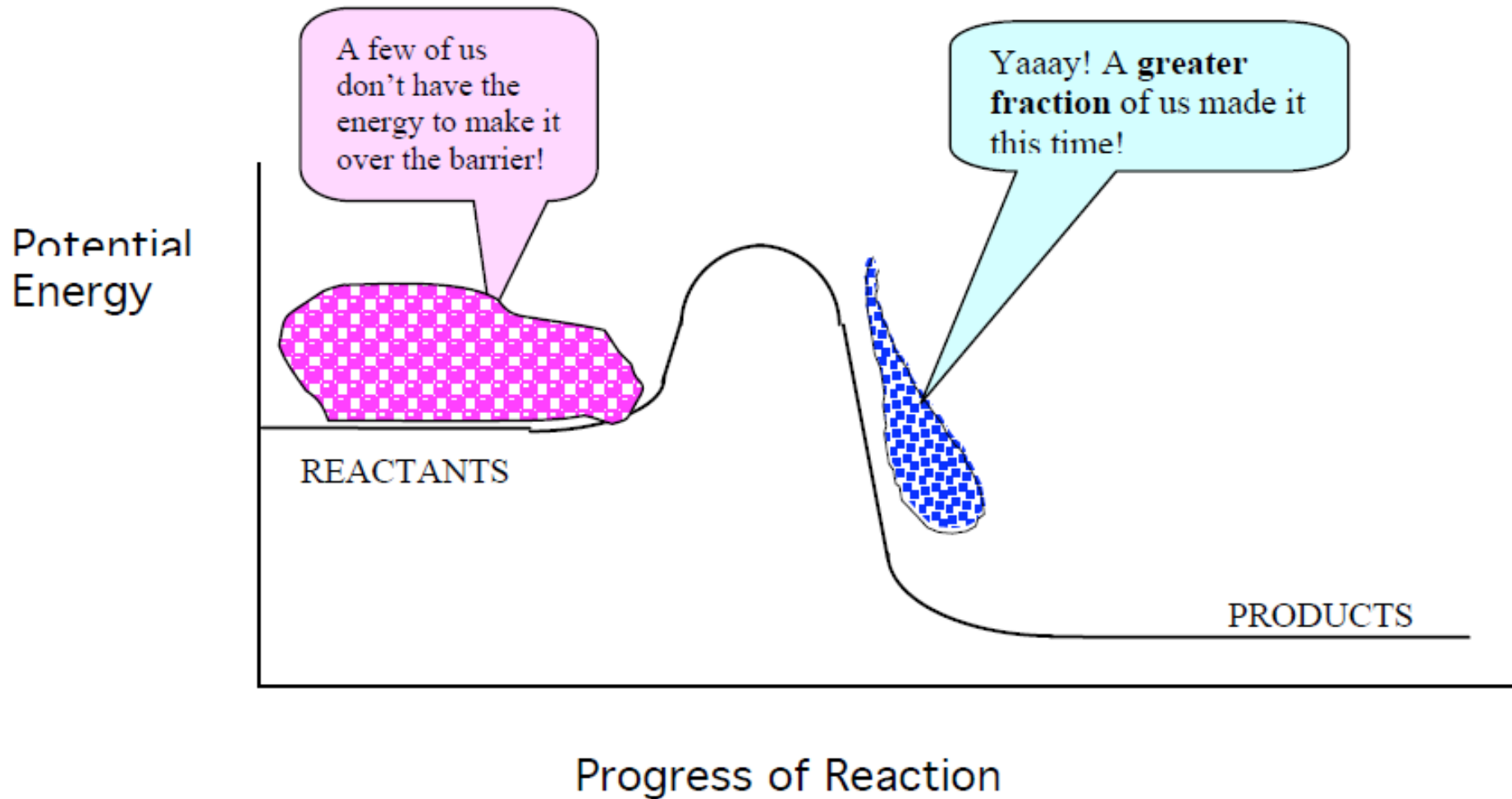
Only a **small fraction** of the molecules had enough energy to overcome the **Activation Energy barrier**.

KE distributions at low T_2



At high T , a greater fraction of the molecules have sufficient energy to “make it over” the Activation Energy barrier.

KE distributions at low T_2



A larger **fraction** of the molecules had enough energy to overcome the Activation Energy barrier.

If you provided a reaction with energy higher than what is required (running at $T_2 > T_1$)

- PEs of reactants and products are supposed to be **unchanged** (do not depend on T but vary with composition or position).
- KE & consequently U and H of reactants increase.
- Reaching TS and moving from TS into products will likely be **faster** because increasing T will increase the particles' collisions.
- PE diagram is not supposed to change with T.
- The **internal energy** and **enthalpy level diagrams** will change based on the impact of **increasing T** on both of reactants and products.

- ▶ The influence of T on KE , U , and H of reactants and products is not necessarily to be the same.
- ▶ At constant P , the change of $\Delta_r H$ ($\Delta_r H_2 - \Delta_r H_1$) with increasing T from T_1 to T_2 depends on $(T_2 - T_1)$ and $\Delta_r C_p$.

$$\Delta_r C_p = \sum_{\text{products}} \nu \Delta C_p - \sum_{\text{reactants}} \nu \Delta C_p$$

where $\nu =$ stoichiometric coefficient of species

Isothermal/adiabatic expansion

- ✦ Typically, any expansion is accompanied by cooling; (losing energy and lowering in system's T)
- ✦ If the system permits heat transfer with surrounding, the system may absorb Q from surrounding to keep its temperature unchanged (isothermal) and $\Delta U=0$.
- ✦ Otherwise, as adiabatic processes, the expansion should result in a lowering of the system T.

$$\Delta U_{isothermal} = Q + W = 0$$

$$\Delta U_{adiabatic} = 0 + W = W$$

Adiabatic expansion, $Q = 0$

$$\Delta U = W = -PdV \quad \rightarrow$$

$$dU = dW = - \int_{V_1}^{V_2} PdV$$

For ideal gases, $P = f(V)$, $n = 1$

$$dU = dW = - \int_{V_1}^{V_2} \frac{RTdV}{V} \quad \rightarrow \quad c_V = \left(\frac{dU}{dT} \right)_V$$

$$\int_{U_1}^{U_2} dU = \int_{T_1}^{T_2} c_V dT = - \int_{V_1}^{V_2} \frac{RTdV}{V}$$

- ▶ Adiabatic: T is not **constant**.
- ▶ **Assume** c_V is independent of T

$$c_V \int_{T_1}^{T_2} \frac{dT}{T} = -R \int_{V_1}^{V_2} \frac{dV}{V}$$

$$c_V \ln \frac{T_2}{T_1} = -R \ln \frac{V_2}{V_1}$$

However,

$$c_P = c_V + R$$

Or

$$R = c_P - c_V$$

Substitute

$$c_V \ln \frac{T_2}{T_1} = -(c_P - c_V) \ln \frac{V_2}{V_1}$$

$$\ln \frac{T_2}{T_1} = - \left(\frac{c_P - c_V}{c_V} \right) \ln \frac{V_2}{V_1}$$

Know

$$\gamma = \frac{c_P}{c_V}$$

$$\ln \frac{T_2}{T_1} = (\gamma - 1) \ln \frac{V_1}{V_2}$$

Note the (V_2 / V_1) flipping



$$\ln \frac{T_2}{T_1} = \ln \left(\frac{V_1}{V_2} \right)^{(\gamma-1)}$$

$$\frac{T_2}{T_1} = \left(\frac{V_1}{V_2} \right)^{(\gamma-1)}$$

$$\ln \frac{T_2}{T_1} = \ln \left(\frac{V_1}{V_2} \right)^{(\gamma-1)} \quad \text{Or}$$

$$T_1 V_1^{(\gamma-1)} = T_2 V_2^{(\gamma-1)}$$

Considering



$$\gamma = \frac{c_P}{c_V} = \frac{c_V + R}{c_V} = 1 + \frac{R}{c_V}$$

$$T_1 V_1^{\left(\frac{R}{c_V}\right)} = T_2 V_2^{\left(\frac{R}{c_V}\right)}$$

Or

$$T_1^{\left(\frac{c_V}{R}\right)} V_1 = T_2^{\left(\frac{c_V}{R}\right)} V_2$$

$$\frac{T_2}{T_1} = \left(\frac{V_1}{V_2}\right)^{(\gamma-1)}$$

For ideal gases

$$\frac{T_2}{T_1} = \frac{P_2 V_2}{P_1 V_1}$$



$$\frac{P_2 V_2}{P_1 V_1} = \left(\frac{V_1}{V_2}\right)^{(\gamma-1)}$$



$$\frac{P_2}{P_1} = \frac{V_1}{V_2} \left(\frac{V_1}{V_2}\right)^{(\gamma-1)}$$

$$\frac{P_2}{P_1} = \left(\frac{V_1}{V_2}\right)^\gamma$$

Or

$$P_1 V_1^\gamma = P_2 V_2^\gamma$$

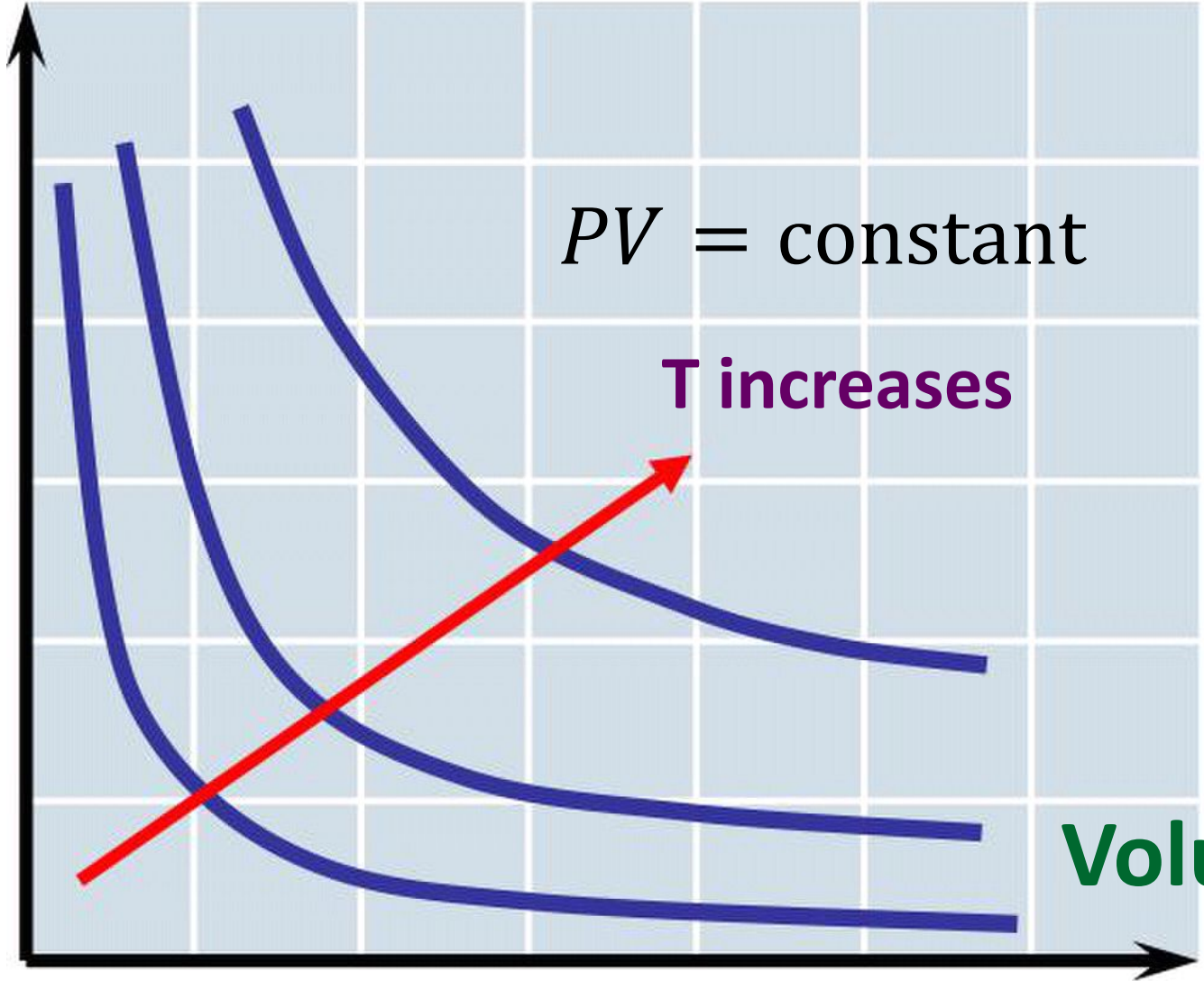
For adiabatic expansion

Compare with isothermal expansion
(Boyl's Law)

$$P_1 V_1 = P_2 V_2$$

Boyle's Law

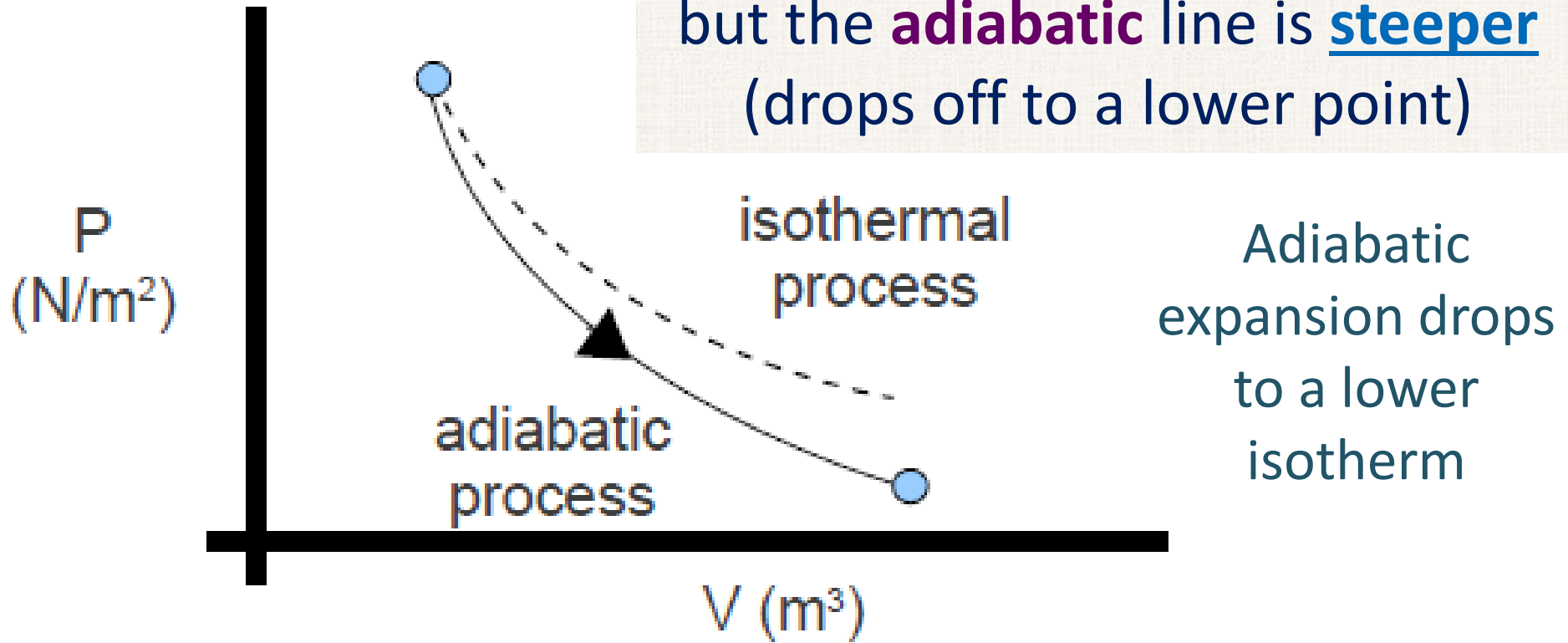
Pressure



As T decreases, the isotherm is shifted downward because of lowering the internal energy.

Isothermal/adiabatic expansion

Their PV diagrams look **similar**, but the **adiabatic** line is steeper (drops off to a lower point)



- ▶ In the adiabatic process where a gas expands, the work done by the gas causes the internal energy to decrease, so the temperature must decrease as well.

Comment

- ✚ On the PV diagrams, the adiabatic change is **steeper** than the isothermal change?

Answer

- ✚ Because the pressure decreases (from P_1 to P_2) more (**inspect it graphically**) in adiabatic processes than in isothermal processes.
- ✚ This is also clear from the derived equation for adiabatic expansion where $\gamma > 1$ in comparison to $\gamma = 1$ in case of isothermal expansion

$$P_1 V_1^\gamma = P_2 V_2^\gamma$$

Ex.

Calculate the work done during an **adiabatic reversible expansion** of 0.85 mole of an ideal mono-atomic gas ($c_v = 12.36 \text{ J mol}^{-1} \text{ K}^{-1}$) from a pressure of 15 atm to 1 atm at 300 K?

Answer

Assume c_v is independent of T , and for ideal gases

$$V_1 = \frac{nRT}{P_1} =$$

$$\frac{(0.85 \text{ mol})(0.82 \text{ L atm K}^{-1} \text{ mol}^{-1})(300 \text{ K})}{15 \text{ atm}} = 1.39 \text{ L}$$

For mono-atomic gas

$$\gamma = \frac{c_p}{c_v} = \frac{5}{3} = 1.67$$

For **adiabatic** expansion of an ideal gas

$$P_1 V_1^\gamma = P_2 V_2^\gamma \quad V_2 = V_1 \left(\frac{P_1}{P_2} \right)^{\frac{1}{\gamma}}$$

$$V_2 = V_1 \left(\frac{P_1}{P_2} \right)^{\frac{1}{\gamma}} = (1.39 \text{ L}) \left(\frac{15}{1} \right)^{\frac{1}{1.69}} = 7.1 \text{ L}$$

$$T_2 = \frac{P_2 V_2}{nR} = \frac{(1 \text{ atm})(7.1 \text{ L})}{(0.85 \text{ mol})(0.82 \text{ L atm K}^{-1} \text{ mol}^{-1})} = 101.2 \text{ K}$$

**Alternatively, To
calculate T_2**



$$\frac{T_2}{T_1} = \left(\frac{V_1}{V_2} \right)^{(\gamma-1)}$$

$$\begin{aligned}
 W &= \Delta U = nc_V(T_2 - T_1) = \\
 &(0.85 \text{ mol})(12.36 \text{ J mol}^{-1}\text{K}^{-1})(101.2 - 300 \text{ K}) \\
 &= -2120 \text{ J}
 \end{aligned}$$

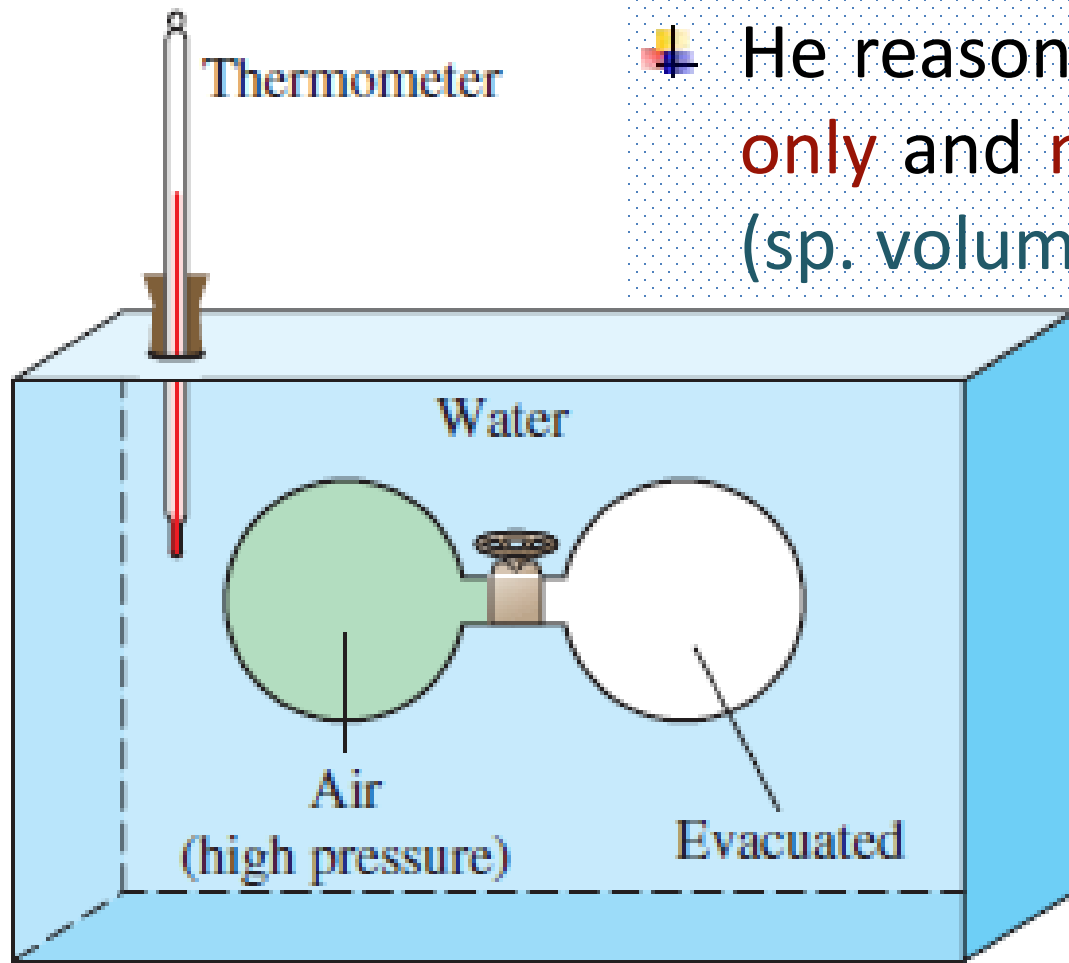
+ If you compared this W with that of **isothermal** reversible expansion of ideal gases, you would notice: $W_{\text{adiabatic}} < W_{\text{isothermal}}$

$$\begin{aligned}
 W_{rev} &= - \int_1^2 P dV = - \int_1^2 \frac{nRT}{V} dV = - P_1 V_1 \ln \frac{V_2}{V_1} \\
 &\left(-(15 \text{ atm})(1.39 \text{ L})(2.303) \log \left(\frac{7.1}{1.39} \right) \right) \left(\frac{101.396 \text{ J}}{\text{L atm}} \right) \\
 &= -3448.28 \text{ J}
 \end{aligned}$$

Joule experiment

$$U = U(T)$$

- ✚ demonstrated for an ideal gas, U depends only on T .
- ✚ He submerged **two tanks** (one containing air at a **high P** and the other was **evacuated**) connected with a pipe and a valve in a water bath.
- ✚ When thermal **equilibrium** was attained, he opened the valve to let air pass from one tank to the other until the pressures equalized.
- ✚ He observed no change in T of water bath and assumed that no **heat** was transferred to or from surrounding air (**adiabatic isolated** process).
- ✚ Since there was also **no work** done (**free expansion**), he concluded that U of the air did not change even though v and P changed.



✚ He reasoned, U is a function of T **only** and **not** a function of P or v (sp. volume)

$$\left(\frac{\partial U}{\partial v}\right)_T = 0$$

Intermolecular forces are **ignored**, and no energy is required to pull gas molecules apart

(**Joule** later showed that for gases that **deviate significantly from ideal gas behavior**, the internal energy is not a function of temperature alone.)

Generally,

$$U = U(T, P, v)$$

- ✚ U of a real gas is a function of P , v , and T .
- ✚ The equation of state (ideal or real gas laws) indicates the possibility of estimating the third variable if two of them were known.
- ✚ is possible to write U in terms of just 2 independent intensive variables: v and T , P and T , or P and v .
- ✚ Expressing U as a function of v and T fits the purpose.

At constant P

$$U = f(v, T)$$

$$dU = \left(\frac{\partial U}{\partial T} \right)_v dT + \left(\frac{\partial U}{\partial v} \right)_T dv = 0$$

Interpretation,

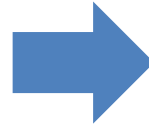
$$dU = \left(\frac{\partial U}{\partial T} \right)_v dT + \left(\frac{\partial U}{\partial v} \right)_T dv = 0$$

- ✚ In a closed system of constant composition, any infinitesimal change in the internal energy is proportional to the infinitesimal changes of volume and temperature.
- ✚ The coefficients of proportionality being the two partial derivatives.

Adiabatic expansion of a gas against vacuum

$$Q = W = dU = 0$$

but



$$\left(\frac{\partial U}{\partial T}\right)_v = c_v$$

$$0 = c_v dT + \left(\frac{\partial U}{\partial v}\right)_T dv$$



$$\left(\frac{\partial U}{\partial v}\right)_T = -c_v \left(\frac{dT}{dv}\right)_U$$

Let us say,

$$\left(\frac{\partial U}{\partial v}\right)_T = \pi_T$$

π_T : internal pressure

- ▶ π_T measures of the variation of U of a substance with its volume at a **constant temperature**.
- ▶ As it has the same dimensions as **pressure**, we will call it the **internal pressure**.
- ▶ This indicates that a change in U of the system as a results of a volume change should be accompanied by a **temperature change**.
- ▶ Lowering U necessitates a **lowering** in T , in case of **expansion**, as a part of U is consumed to overcome intermolecular forces between gas particles (Real gas perspective) to permit **expansion**. Reverse is true for **compression**.

- ▶ The temperature change accompanying a gas expansion is given by

$$\left(\frac{dT}{dv}\right)_U = \frac{-1}{c_v} \left(\frac{\partial U}{\partial v}\right)_T = \frac{-\left(\frac{\partial U}{\partial v}\right)_T}{\left(\frac{\partial U}{\partial T}\right)_v}$$

For real gas

- ▶ A temperature change accompanying a gas expansion should be on the expense of the internal energy (This is true for real gases).
- ▶ For ideal gases, intermolecular forces are neglected, and Joule's conclusion is valid.

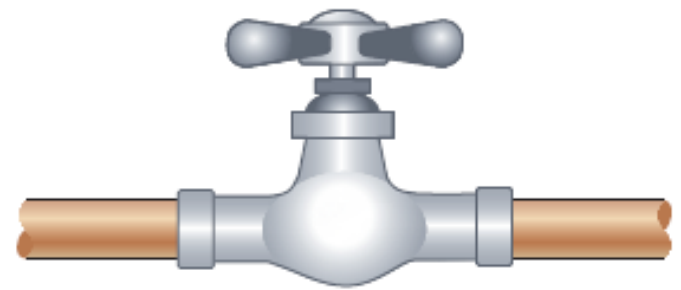
$$\left(\frac{\partial U}{\partial v}\right)_T = 0 = \left(\frac{dT}{dv}\right)_U$$

- ▶ An ideal gas can, therefore, be defined as the gas whose **energy** at **constant temperature** is independent of its **volume**

$\left(\frac{dT}{dv}\right)_U$ is called the **Joule coefficient**

Throttling valves

- are **flow-restricting** devices that cause a significant **pressure drop** in fluids, e.g., ordinary adjustable valves, capillary tubes, & porous plugs.
- They produce a **pressure drop** without involving any work.



(a) An adjustable valve



(b) A porous plug



(c) A capillary tube

- The pressure drop in the fluid is often accompanied by a large drop in temperature, and for that reason throttling devices are commonly used in refrigeration and air-conditioning applications.

- ▶ The magnitude of the **temperature drop** (or, sometimes, the **temperature rise**) during a throttling process is governed by a property called the **Joule-Thomson coefficient**.
- ▶ **Throttling valves** are usually small devices, and the flow through them may be assumed to be **adiabatic** ($Q \approx 0$) since there is neither **sufficient time** nor **large enough area** for any effective **heat transfer** to take place.
- ▶ Also, there is **no work done** ($W = 0$), and the change in potential energy, if any, is very small ($\Delta pe \approx 0$).
- ▶ Even though the **exit velocity** is often considerably **higher** than the **inlet velocity**, in many cases, the increase in kinetic energy is insignificant ($\Delta ke \approx 0$).

Energy Conservation in Throttling valves

- ✚ For this **single-stream** steady-flow device, energy conservation reduces to $H_2 \approx H_1$, i.e., H values at the inlet and exit of a throttling valve are the same.
- ✚ For throttling devices with **large** exposed **surface areas** such as capillary tubes, heat transfer may be significant.

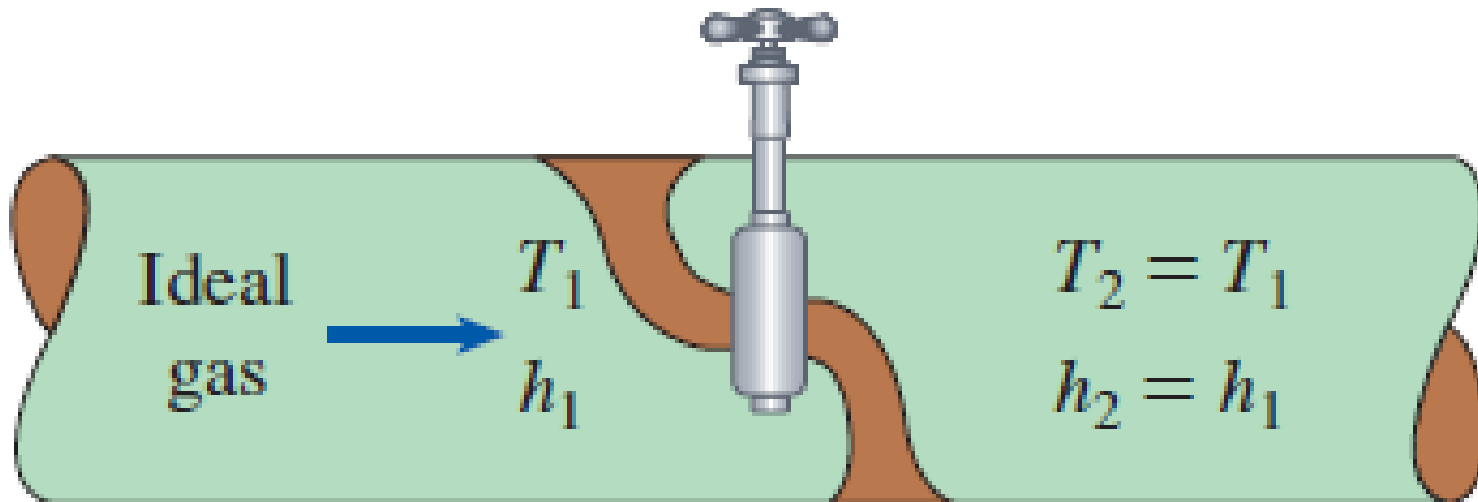
$$H_1 = H_2$$

$$U_1 + P_1 v_1 = U_2 + P_2 v_2$$

- ▶ The **outcome** of a throttling process depends on which of the two quantities increases in the process.
- ▶ If the **flow energy** ($Pv = \frac{P}{\rho}$) **increases** during the process ($P_2 v_2 > P_1 v_1$), **internal energy** must **decrease**, which is usually accompanied by a **drop in T**.

- ▶ If the product Pv decreases, the internal energy and the temperature of a fluid will increase during a throttling process.
- ▶ In the case of an ideal gas, $H = H(T)$, and thus the temperature must remain constant during a throttling process.

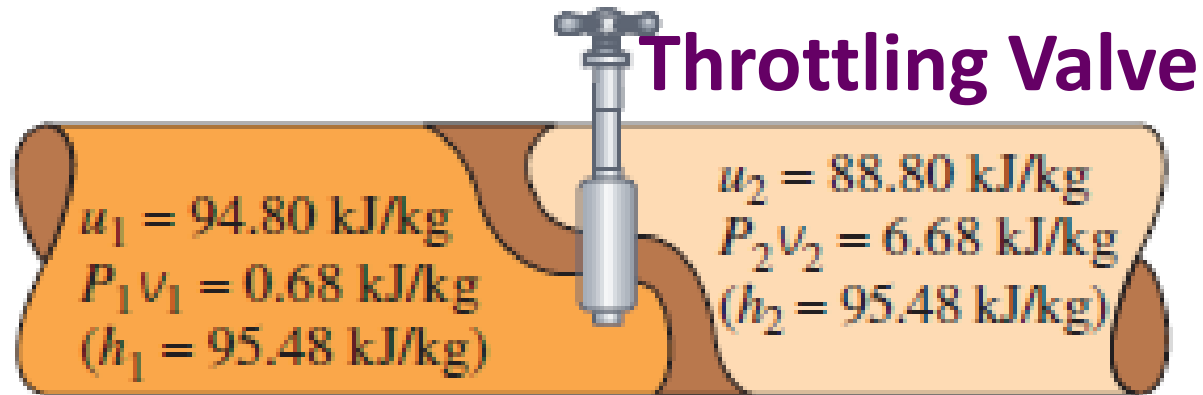
Throttling Valve



Ex.

Refrigerant-134a enters the capillary tube of a refrigerator as **saturated liquid** at **0.8 MPa** and is throttled to a pressure of **0.12 MPa**. Determine the **quality** of the refrigerant at the final state and the temperature drop during this process?

Answer



Saturated refrigerant-134a—Pressure table

Press., P kPa	Sat. temp., T_{sat} °C	Specific volume, m^3/kg		Internal energy, kJ/kg			Enthalpy, kJ/kg			Entropy, kJ/kg·K		
		Sat. liquid, v_f	Sat. vapor, v_g	Sat. liquid, u_f	Evap., u_{fg}	Sat. vapor, u_g	Sat. liquid, h_f	Evap., h_{fg}	Sat. vapor, h_g	Sat. liquid, s_f	Evap., s_{fg}	Sat. vapor, s_g

120	-22.32	0.0007323	0.16216	22.38	195.15	217.53	22.47	214.52	236.99	0.09269	0.85520	0.94789
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800	31.31	0.0008457	0.025645	94.80	152.02	246.82	95.48	171.86	267.34	0.35408	0.56445	0.91853
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► Flow through a capillary tube is a **throttling** process; thus, the **enthalpy** of the refrigerant remains constant.

At inlet: (sat. liquid or fluid)

$$P_1 = 0.8 \text{ MPa}$$

$$T_1 = T_{\text{sat}} @ 0.8 \text{ MPa} = 31.31^\circ\text{C}$$

$$h_1 = h_f @ 0.8 \text{ MPa} = 95.48 \text{ kJ/kg}$$

At exit: (sat. liquid or fluid)

$$P_2 = 0.12 \text{ MPa}$$

$$T_{\text{sat}} = -22.32^\circ\text{C}$$

$$h_f = 22.47 \text{ kJ/kg}$$

$$h_g = 236.99 \text{ kJ/kg}$$

► $h_2 = h_1 = 95.48 \text{ kJ/kg}$, a value between $h_f < h_2 < h_g$

► Thus, the refrigerant exists as a **saturated mixture** at the exit state.

- ▶ The quality, χ_2 , at this state is

$$\chi_2 = \frac{h_2 - h_f}{h_{fg}} = \frac{95.48 - 22.47}{236.99 - 22.47} = 0.340$$

- ▶ Since the exit state is a **saturated mixture** at **0.12 MPa**, the exit temperature must be the saturation temperature at this pressure, which is **-22.32°C** .
- ▶ Then the temperature change for this process becomes

$$\Delta T = T_2 - T_1 = (-22.32 - 31.31)^\circ\text{C} = -53.63^\circ\text{C}$$

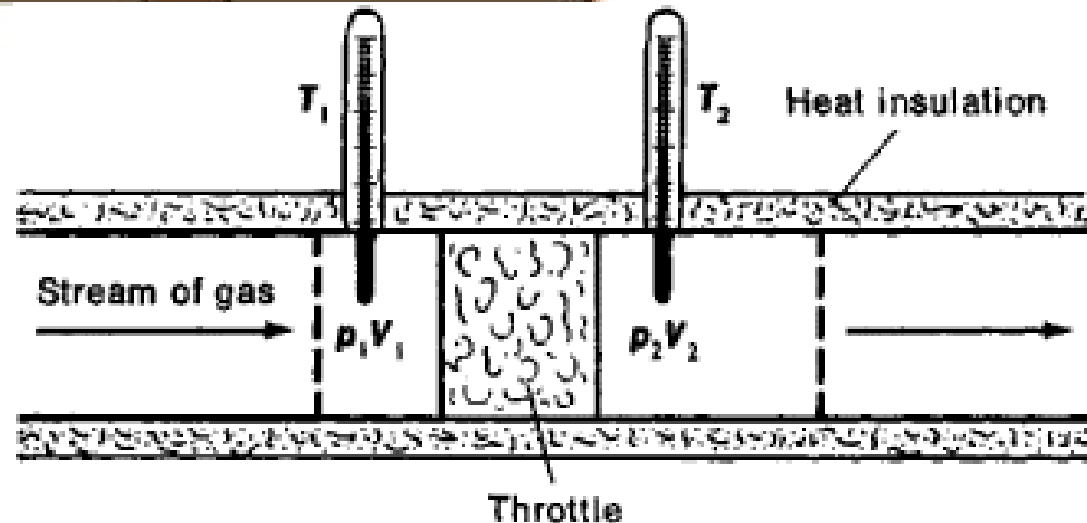
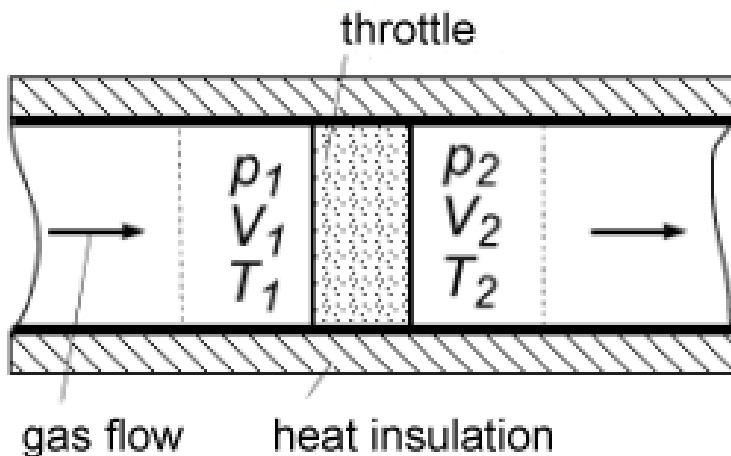
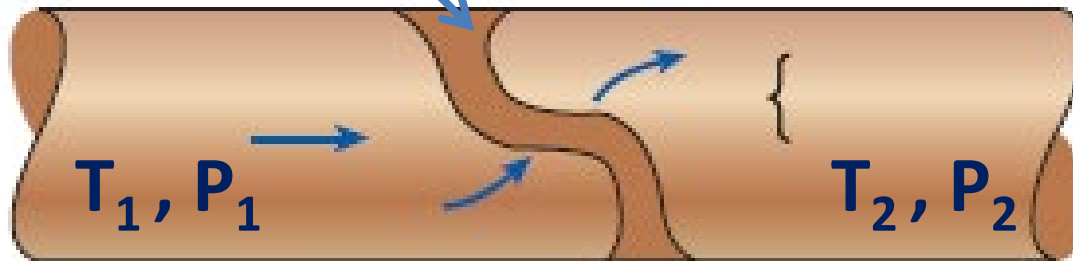
Note that

- ▶ T of the refrigerant drops by **53.63°C** .
- ▶ **34.0 percent** of the refrigerant **vaporizes** during this throttling process and the energy needed to vaporize this refrigerant is absorbed from **refrigerant** itself.

Joule-Thomson effect

- When a fluid passes through a **restriction** such as a **porous plug**, a capillary tube, or an ordinary valve, its pressure **decreases**.

Porous plate  **Insulation**



- ▶ The **enthalpy** of the fluid remains approximately **constant** during such a throttling process.
- ▶ A fluid may experience a **large drop** in its temperature as a result of throttling. This is not always the case.
- ▶ The temperature of the fluid may remain **unchanged**, or it may even **increase** during a throttling process.

The temperature behavior of a fluid during a throttling ($H = \text{constant}$) process is described by the **Joule-Thomson coefficient**, defined as

$$\mu = \left(\frac{\partial T}{\partial P} \right)_H$$

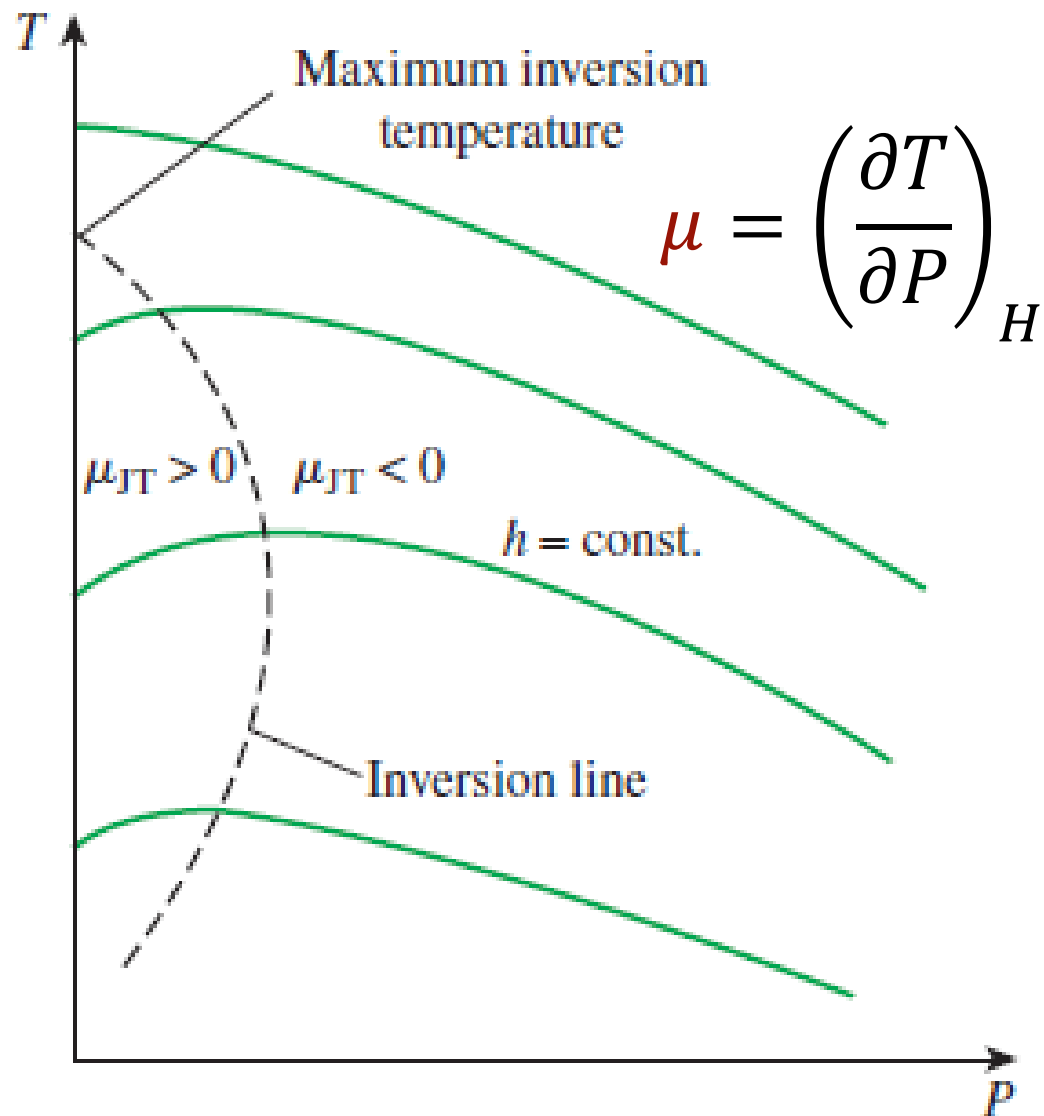
- < 0, T increases
- = 0, T remains constant
- > 0, T decreases

- # The Joule-Thomson coefficient represents the **slope of $h = \text{constant}$** lines on a **T-P diagram**.
- # A fluid at a fixed temperature and pressure T_1 and P_1 (thus **fixed enthalpy**) is forced to flow through a porous plug, and its temperature and pressure downstream (T_2 and P_2) are measured.
- # The experiment is repeated for **different sizes of porous plugs**, each giving a different set of T_2 and P_2 .
- # Plotting the temperatures against the pressures gives us an **$h = \text{constant}$** line on a **T-P diagram**.
- # Repeating the experiment for **different sets of inlet pressure and temperature** and plotting the results, we can construct a **T-P diagram** for a substance with several **$h = \text{constant}$** lines.

Some constant-enthalpy lines pass through a point of **zero slope** or **zero μ** .

The line that passes through these points is called the **inversion line**.

The temperature at a point where a constant-enthalpy line intersects the inversion line is called the **inversion temperature**.



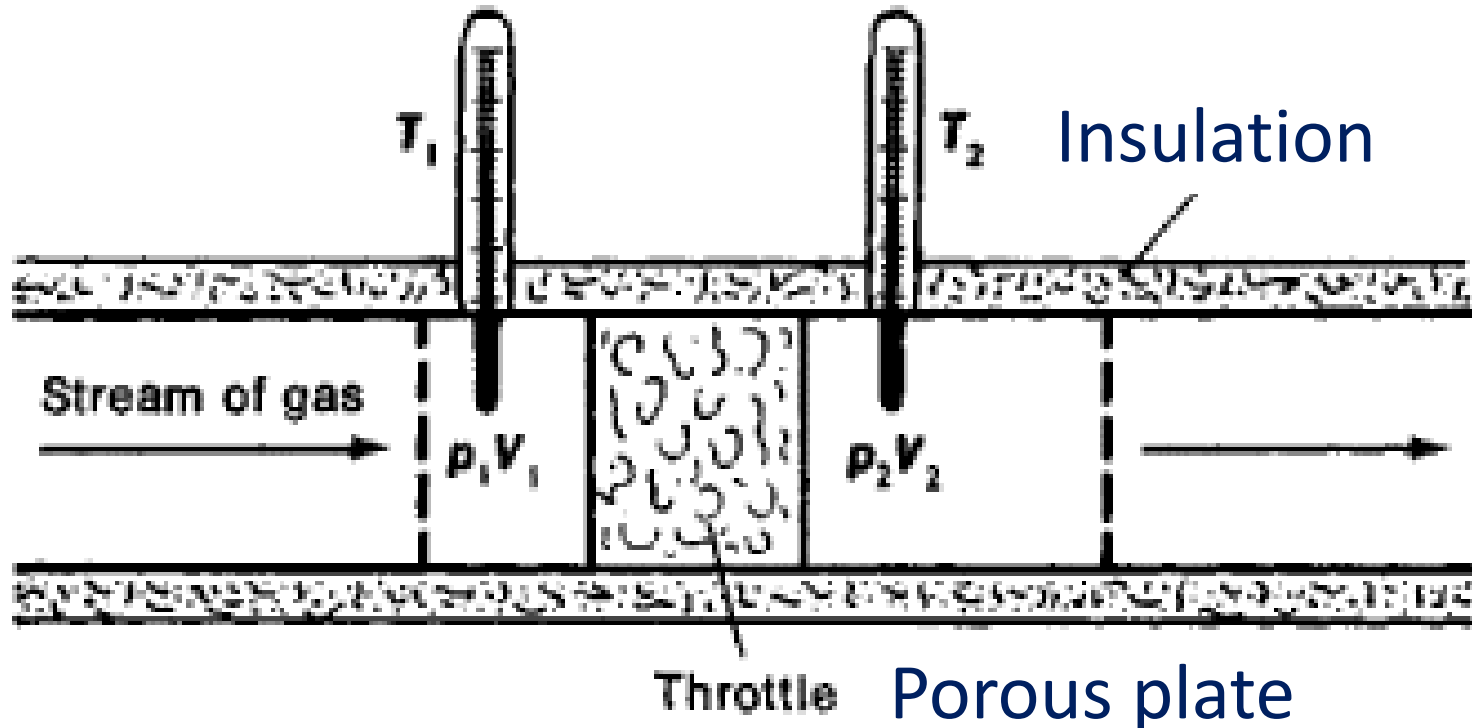
Constant-enthalpy lines of a substance on a T-P diagram.

- # The T at the intersection of the $P = 0$ line (ordinate) and the upper part of the inversion line is called the **maximum inversion temperature**.
- # Notice that the **slopes** of the **$h = \text{constant}$** lines are negative ($\mu < 0$) at states to the right of the inversion line and positive ($\mu > 0$) to the left of the inversion line.
- # A throttling process proceeds along a constant-enthalpy line in the direction of **decreasing pressure**, that is, from right to left.
- # Therefore, the temperature of a fluid **increases** during a throttling process that takes place on the right-hand side of the **inversion line**.
- # However, the **fluid temperature decreases** during a throttling process that takes place on the left-hand side of the **inversion line**.

- ✚ It is clear from this diagram that a **cooling effect** cannot be achieved by throttling unless the fluid is below its **maximum inversion temperature**.
- ✚ This presents a problem for substances whose **maximum inversion temperature** is well below room temperature.
- ✚ For **hydrogen**, for example, the maximum inversion temperature is -68°C . Thus, it must be cooled below this temperature if any further cooling is to be achieved by throttling. **Hydrogen shows exceptionally a heating effect. Comment?**

Mathematically

- By applying a pressure on the left side (piston) so slowly that no change in P_1 occurs but a volume of gas V_1 passes slowly through the porous plug to expand in the right compartment to V_2



- The **work** done on the system at the left piston is P_1V_1 and the work done by the system at the right piston is P_2V_2 .
- The net work done on the system is given by

$$W = (P_1V_1 - P_2V_2) = -(P_2V_2 - P_1V_1)$$

- For adiabatic expansion, $Q = 0$ and $\Delta U = W$.

$$U_2 - U_1 = -P_2V_2 + P_1V_1$$

$$U_2 + P_2V_2 = U_1 + P_1V_1$$

$$H_2 = H_1$$

$$\Delta H = 0$$

Adiabatic processes occurs under **constant enthalpy**

- Joule & Thomson observed that all real gases (**except H_2**) undergo **cooling** during adiabatic expansion.

- ΔT depends on the initial conditions (T , P of the gas, which identify the system enthalpy that will remain constant during expansion).
- The Joule-Thomson coefficient (μ) is give by:

$$\mu = \left(\frac{\partial T}{\partial P} \right)_H$$

$$H = H(T, P)$$

Consider an **adiabatic expansion** of a real gas

$$dH = 0$$

$$dH = \left(\frac{\partial H}{\partial T} \right)_P dT + \left(\frac{\partial H}{\partial P} \right)_T dP = 0$$

$$\left(\frac{\partial H}{\partial T} \right)_P = c_P$$

$$c_P dT + \left(\frac{\partial H}{\partial P} \right)_T dP = 0$$

$$\left(\frac{dT}{dP} \right)_H = -\frac{1}{c_P} \left(\frac{\partial H}{\partial P} \right)_T$$

$$\mu = -\frac{1}{c_P} \left(\frac{\partial H}{\partial P} \right)_T = -\frac{1}{c_P} \left(\frac{\partial (U + Pv)}{\partial P} \right)_T$$

$$\mu = -\frac{1}{c_P} \left(\frac{\partial U}{\partial P} \right)_T - \frac{1}{c_P} \left(\frac{\partial Pv}{\partial P} \right)_T$$

$$\left(\frac{\partial U}{\partial P} \right)_T$$

is always
-ve

- ▶ Because for real gases, work is done against the intermolecular attraction during expansion
- ▶ In adiabatic expansion **P decreases** and T decreases. In order to keep T constant, the system should receive work from surrounding to **increase U**

$$\mu = -\frac{1}{C_P} \left(\frac{\partial U}{\partial P} \right)_T - \frac{1}{C_P} \left(\frac{\partial Pv}{\partial P} \right)_T$$

► Therefore, the first term of the above equation leads to cooling effect.

$$\left(\frac{\partial Pv}{\partial P} \right)_T \begin{cases} < 0, \text{ at low } P & \longrightarrow \text{cooling } / +\text{Ve } \mu \\ > 0, \text{ at High } P & \longrightarrow \text{Heating } / -\text{Ve } \mu \end{cases}$$

Inversion Temperature

The **temperature** at which the **cooling effect** of the first term is equal the **heating effect** of the second term and thus $\mu=0$.

- At this temperature, the gas will not undergo a temperature change on expansion.
- Above the inversion temperature, the gas undergoes a heating effect upon expansion.
- Below the inversion temperature, the gas undergoes a cooling effect upon expansion.