

# Thermodynamics



Chem 211: **Lecture 10**

*Thermodynamics of*

**Phase Equilibria**

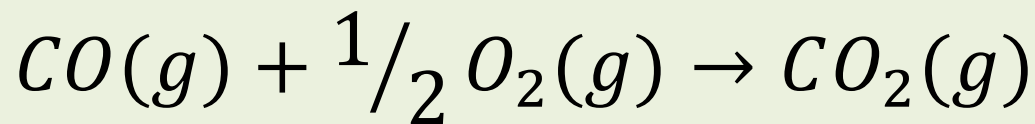
**Ahmad Alakraa**

# Standard molar Gibbs energies

$$\Delta_r G^0 = \Delta_r H^0 - T \Delta_r S^0$$

$$\Delta_r G^0 = \sum_{\text{Products}} \nu \Delta_f G^0 - \sum_{\text{Reactants}} \nu \Delta_f G^0$$

For the Rx



$$\Delta_r G^0 = \Delta_f G^0(CO_2) - \Delta_f G^0(CO) - \frac{1}{2} \Delta_f G^0(O_2)$$

$$\Delta_r G^0$$

$$= -394.4 \text{ kJ mol}^{-1} - \left( -137.2 - \frac{1}{2} (0) \right) \text{ kJ mol}^{-1}$$

$$= -257.2 \text{ kJ mol}^{-1}$$

# Criteria of Reversibility

For a change in a closed system of constant composition, and in the absence of any additional (non-expansion) work

Irreversible	Reversible
$(dS)_{V,U} > 0$	$(dS)_{V,U} = 0$
$(dU)_{V,S} < 0$	$(dU)_{V,S} = 0$
$(dH)_{P,S} < 0$	$(dH)_{P,S} = 0$
$(dS)_{P,H} > 0$	$(dS)_{P,H} = 0$
$(dA)_{T,V} < 0$	$(dA)_{T,V} = 0$
$(dG)_{T,P} < 0$	$(dG)_{T,P} = 0$

# Combining 1<sup>st</sup> and 2<sup>nd</sup> Laws of Thermodynamics

# Fundamental equations

✚ For a **reversible** change in a **closed system** of **constant composition**, and in the **absence** of any additional (non-expansion) work,

$$dU = dQ + dW$$

$$dW_{rev} = -PdV$$

$$dQ_{rev} = TdS$$


$$dU = TdS - PdV$$

**Fundamental Equation**

**Note:**  $\Delta U$  is path independent

# Partial molal free energy, $\bar{G}_1$

As  $G$  is an extensive state property, thus for a system containing several components at constant  $T, P$ :

$$dG_{sys} = \sum dG_{components} = n_1 \bar{G}_1 + n_2 \bar{G}_2 + \dots$$

$\bar{G}_1$  : the increase in the total free energy of the system upon increasing  $n_1$  by 1 mol while keeping other variables ( $n_2, n_3, \dots$  etc,  $P$  and  $T$ ) constant.

$$\bar{G}_1 = \left( \frac{\partial G_{sys}}{\partial n_1} \right)_{n_2, n_3, \dots, T, P}$$

# Chemical Potential, $\mu$

- ✚ For a pure substance (one component only),  $\bar{G}_1$  is simply the free energy per mole, molar Gibb's free energy.
- ✚ In solutions,  $\bar{G}_1$  is called the chemical potential,  $\mu_1$ .

$$\mu_1 = \left( \frac{\partial G_{sys}}{\partial n_1} \right)_{n_2, n_3, \dots, T, P}$$

For an ideal gas

$$\mu = \mu_0 + RT \ln P$$

- ✚  $\mu_0$  is the standard (1 atm, 298 K) chemical potential.

For a real gas

$$\mu = \mu_0 + RT \ln f$$

$f$  : fugacity or effective pressure

# Effect of T and P on G

$$dG = VdP - SdT$$

**+ve**  $\left(\frac{\partial G}{\partial P}\right)_T = V$

$\left(\frac{\partial G}{\partial T}\right)_P = -S$  **-ve**

✚ This equation was derived for systems containing one component of **fixed composition** and assuming only **PV work**. If components and composition are changed during the process, then,

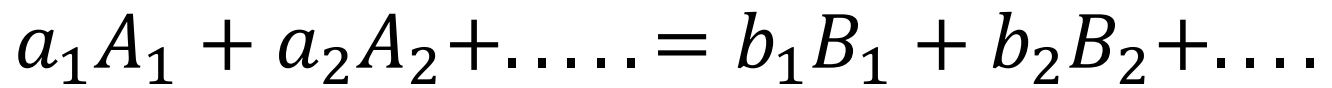
$$dG = VdP - SdT + \mu_1 dn_1 + \mu_2 dn_2 + \dots$$

**If other work is assumed**

$$dG = Vdp + EdQ - SdT + \mu_1 dn_1 + \mu_2 dn_2 + \dots$$

**Or**  $dG = Vdp + \gamma d\sigma - SdT + \mu_1 dn_1 + \mu_2 dn_2 + \dots$

**Consider  
this Rx**



$$\Delta G = \sum G_{\text{products}} - \sum G_{\text{reactants}}$$

$$\Delta G = [b_1G_{B_1} + b_2G_{B_2} + \dots] - [a_1G_{A_1} + a_2G_{A_2} + \dots]$$

$$\left(\frac{d\Delta G}{dP}\right)_T = \Delta V$$

$$\left(\frac{d\Delta G}{dT}\right)_P = -\Delta S$$

- ✚ If a reaction proceeds with **no change in volume** between reactants and products at **constant T**,  $\Delta G$  will be **independent** of P.
- ✚ If a reaction proceeds with **no change in entropy** between reactants and products at **constant P**,  $\Delta G$  will be **independent** of T.

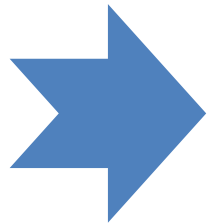
# Effect of T on G

Consider the differentiation of  $G/T$  with respect to  $T$

$$\left( \frac{d(G/T)_P}{dT} \right) = \frac{1}{T} \left( \frac{\partial G}{\partial T} \right)_P - \frac{G}{T^2}$$

Utilizing these formulas  $\left( \frac{\partial G}{\partial T} \right)_P = -S$  and  $G = H - TS$

$$\left( \frac{d(G/T)_P}{dT} \right) = \frac{-S}{T} - \left( \frac{H}{T^2} - \frac{S}{T} \right) = -\frac{H}{T^2}$$

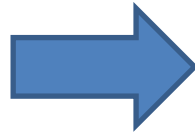


$$\left( \frac{d(\Delta G/T)_P}{dT} \right) = -\frac{\Delta H}{T^2}$$

# Effect of T on A

$$dA = -PdV - SdT$$

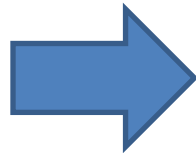
Isochoric (const. V) processes



$$\left(\frac{dA}{dT}\right)_V = -S$$

$$\left(\frac{d\Delta A}{dT}\right)_V = -\Delta S$$

Isothermal Processes



$$\left(\frac{dA}{dV}\right)_T = -P$$

$$\left(\frac{d\Delta A}{dV}\right)_T = -\Delta P$$

$$\Delta A = \Delta U + T \left(\frac{d\Delta A}{dT}\right)_V$$

$$\left(\frac{d(\Delta A/T)_V}{dT}\right) = -\frac{\Delta U}{T^2}$$

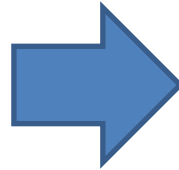
# Gibbs-Helmholtz equation

For isothermal processes

$$\Delta G = \Delta H - T\Delta S$$

Utilizing this formula

$$\left(\frac{d\Delta G}{dT}\right)_P = -\Delta S$$



$$\Delta G = \Delta H + T \left(\frac{d\Delta G}{dT}\right)_P$$

# Gibbs-Helmholtz equation

# Kinetic limited/controlled Rx

✚ are reactions having a **negative  $\Delta G$** , yet they do not proceed spontaneously unless a **barrier** is **overcome** (energy is provided to initiate the Rx) by adding a catalyst.

✚ **Example,**



✚ Just mixing of  $\text{H}_2(\text{g})$  and  $\text{O}_2(\text{g})$  do not produce unless a catalyst (**electric spark**, **platinized asbestos**) is added.

✚ A  **$-Ve \Delta G$**  measures the driving force of reactions when these reactions occur.

✚ The catalyst does not affect  **$\Delta G$**  (path independent).

# Gibb's equation

# Interpretation

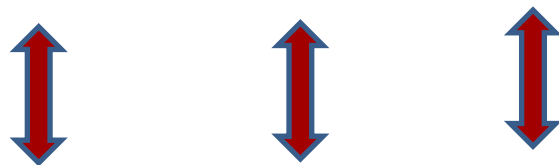
Criterion of spontaneity is the increase in the total entropy.

$$\Delta S_t = \Delta S_{sur} + \Delta S_{sys}$$

For chemical reactions (endothermic or exothermic),

$$\Delta S_{sur} = \frac{-Q_P}{T} = \frac{-\Delta H}{T} \quad \longrightarrow \quad \Delta S_t = \frac{-\Delta H}{T} + \Delta S_{sys}$$

$$-T\Delta S_t = \Delta H - T\Delta S_{sys}$$



$$\Delta G = \Delta H_{sys} - T\Delta S_{sys}$$

$$\Delta G = -T\Delta S_t$$

# *Thermodynamics of Phase Equilibria*

# Phase Eq. in pure substances

**Consider** the following equilibrium



- ✚ **Equilibrium** means that  $\Delta G_{P,T} = G_2 - G_1 = 0$ .
- ✚ If equilibrium is interrupted **infinitesimally** (small reversible change,) by changing P or T, equilibrium will be restored quickly.

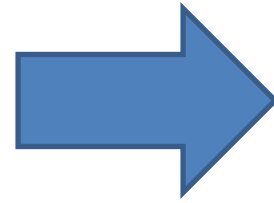
$$dG_1 = dG_2$$

$$V_1 dP - S_1 dT = V_2 dP - S_2 dT$$

$$\frac{dP}{dT} = \frac{S_2 - S_1}{V_2 - V_1} = \frac{\Delta S}{\Delta V}$$

Since the phase change occurs reversibly and isothermally,

$$\Delta S = \frac{\Delta H}{T}$$



$$\frac{dP}{dT} = \frac{\Delta S}{\Delta V} = \frac{\Delta H}{T\Delta V}$$

$$\frac{dT}{dP} = \frac{T\Delta V}{\Delta H}$$

## Clapeyron's equation

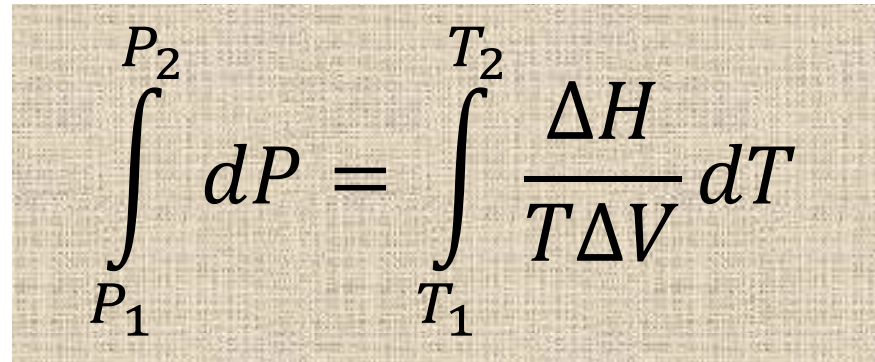
Phase diagrams

- ▶ It represents the effect of **pressure** on the **equilibrium temperature** of phase transformations.
- ▶ It helps in calculating the **vapor pressure** of liquids and sublimating solids.


# Effect of P on equilibrium T

- ✚ **Heterogeneous equilibria** always occur at specified T (i.e., isothermally) and associated by  $\Delta H$  and  $\Delta V$ .
- ✚ The eq. T of a given reaction can be calculated at a given pressure as following:

$$\frac{dP}{dT} = \frac{\Delta H}{T\Delta V}$$


$$\int_{P_1}^{P_2} dP = \int_{T_1}^{T_2} \frac{\Delta H}{T\Delta V} dT$$

- ▶ If  $\Delta H$  and  $\Delta V$  as functions of T are known, we can substitute easily. Otherwise, assume them **independent of T** over a limited small range of T


$$\int_{P_1}^{P_2} dP = \frac{\Delta H}{\Delta V} \int_{T_1}^{T_2} \frac{dT}{T}$$

$$P_2 - P_1 = \frac{\Delta H}{\Delta V} \ln \left( \frac{T_2}{T_1} \right)$$

**P vs. ln T is linear**

# Exercise

The **densities** of liquid and solid Hg are listed below at the melting point and 1 atm. The latent heat of fusion is also given at melting point. Find the rate of changing the melting point with pressure ( $^{\circ}\text{C atm}^{-1}$ ) and calculate the melting point at 50 atm?

Eq.	$d_1,$ $\text{g cm}^{-3}$	$V_1,$ $\text{cm}^3\text{g}^{-1}$	$d_2,$ $\text{g cm}^{-3}$	$V_2,$ $\text{cm}^3\text{g}^{-1}$	$\Delta H, \text{cal}$ $\text{mol}^{-1}$	$T_{eq}, ^{\circ}\text{C}$
$\text{Hg}_{(s)} \leftrightarrow \text{Hg}_{(l)}$	14.19		13.7		566	-38.87

# Solution

$V = \text{specific volume} \times \text{atomic mass}$

As  $\Delta H$  is given in cal/mol,  $V$  is the molar volume

<i>Eq.</i>	$d_1,$ $g\ cm^{-3}$	$V_1,$ $cm^3g^{-1}$	$d_2,$ $g\ cm^{-3}$	$V_2,$ $cm^3g^{-1}$	$\Delta H,$ <i>cal</i> <i>mol</i> <sup>-1</sup>	$T_{eq},$ °C
$Hg_{(s)} \leftrightarrow Hg_{(l)}$	<b>14.19</b>	<b>0.070</b>	<b>13.7</b>	<b>0.073</b>	<b>566</b>	<b>-38.87</b>

$$V_1 = \left( \frac{0.070\ cm^3}{g} \right) \left( \frac{200.5\ g}{mol} \right) = \frac{14.1297\ cm^3}{mol}$$

$$V_2 = \left( \frac{0.073\ cm^3}{g} \right) \left( \frac{200.5\ g}{mol} \right) = \frac{14.6350\ cm^3}{mol}$$

$$\Delta V = V_2 - V_1 = \frac{0.5056\ cm^3}{mol}$$

$$\begin{aligned}\frac{dT}{dP} &= \frac{T\Delta V}{\Delta H} = \frac{(234.28K) \left(\frac{0.5056 \text{ cm}^3}{\text{mol}}\right)}{\left(\frac{566 \text{ cal}}{\text{mol}}\right) \left(\frac{41.268 \text{ cm}^3 \text{ atm}}{\text{cal}}\right)} \\ &= 0.00507 \text{ K atm}^{-1} = 0.00507 \text{ }^\circ\text{C atm}^{-1}\end{aligned}$$

- ▶ As we are concerning with change in T, therefore a change in  $^\circ\text{C}$  is the same as in  $\text{K}$ .
- ▶ The mp increases by  $0.00507 \text{ K}$  per  $\text{atm}$ .

$$P_2 - P_1 = \frac{\Delta H}{\Delta V} \ln \left( \frac{T_2}{T_1} \right)$$

$$\begin{aligned} & 50 \text{ atm} - 1 \text{ atm} \\ &= \frac{\left( \frac{566 \text{ cal}}{\text{mol}} \right) \left( \frac{41.268 \text{ cm}^3 \text{ atm}}{\text{cal}} \right)}{\left( \frac{0.5056 \text{ cm}^3}{\text{mol}} \right)} \ln \left( \frac{T_2}{234.28 \text{ K}} \right) \end{aligned}$$

$$T_2 = 234.53 \text{ K}$$

- Note this **minute change in T (mp)** with this large change in p

# Homework

Use the same data of Hg to calculate the pressure at which the mp of Hg is 1 °C higher than its mp at 1 atm?

Eq.	$d_1,$ $g\ cm^{-3}$	$V_1,$ $cm^3g^{-1}$	$d_2,$ $g\ cm^{-3}$	$V_2,$ $cm^3g^{-1}$	$\Delta H,$ cal $mol^{-1}$	$T_{eq},$ °C
$Hg_{(s)} \leftrightarrow Hg_{(l)}$	14.19		13.7		566	-38.87

# Reference data at 1 atm

Substance	Standard (0 °C) Latent Heat of Fusion kJ/kg	Standard (100 °C) Latent Heat of Vaporization kJ/kg
Water	334.56	2264.76

# Ice/water equilibrium



Eq.	$d_1$ $\text{g cm}^{-3}$	$V_1$ $\text{cm}^3 \text{g}^{-1}$	$d_2$ $\text{g cm}^{-3}$	$V_2$ $\text{cm}^3 \text{g}^{-1}$	$\Delta H$ , kJ $\text{g}^{-1}$	$T_{eq}$ K
$H_2O_{(s)} \leftrightarrow H_2O_{(l)}$	<b>0.916</b>	<b>1.0907</b>	<b>0.9999</b>	<b>1.0001</b>	<b>334.56</b>	<b>273</b>

$$\frac{dT}{dP} = \frac{T\Delta V}{\Delta H} = \frac{(273\text{K}) \left( \frac{-0.0906 \text{ cm}^3}{\text{g}} \right)}{\left( \frac{334.56 \text{ J}}{\text{g}} \right) \left( \frac{1 \text{ L atm}}{101.39 \text{ J}} \right) \left( \frac{1000 \text{ cm}^3}{\text{L}} \right)} =$$

$$= -7.4957 \times 10^{-03} \text{ K atm}^{-1}$$

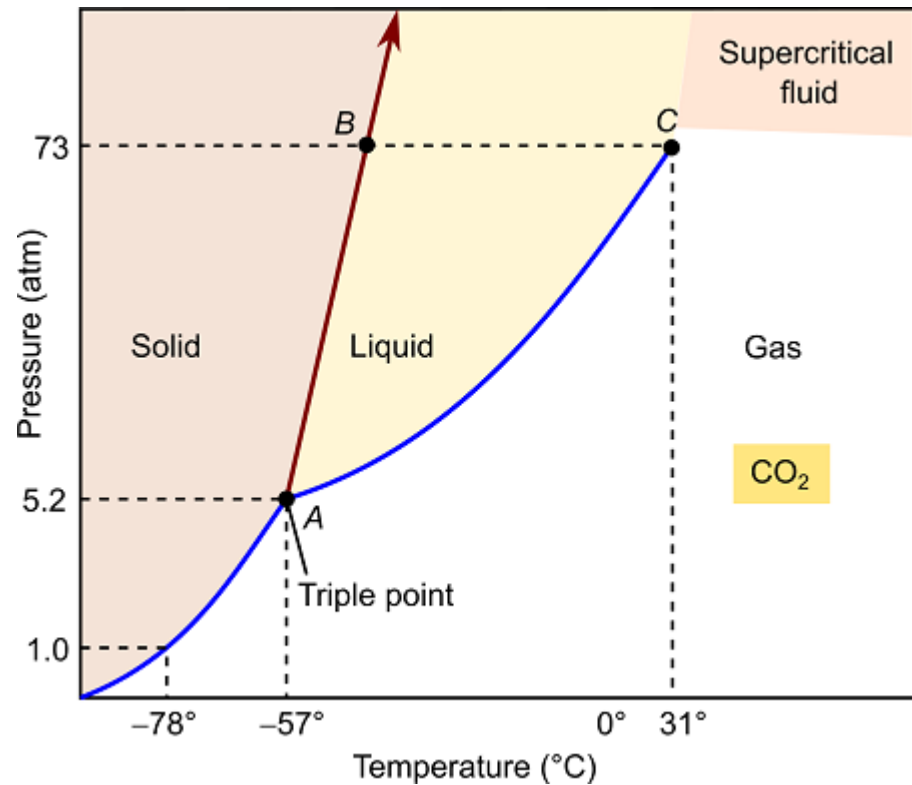
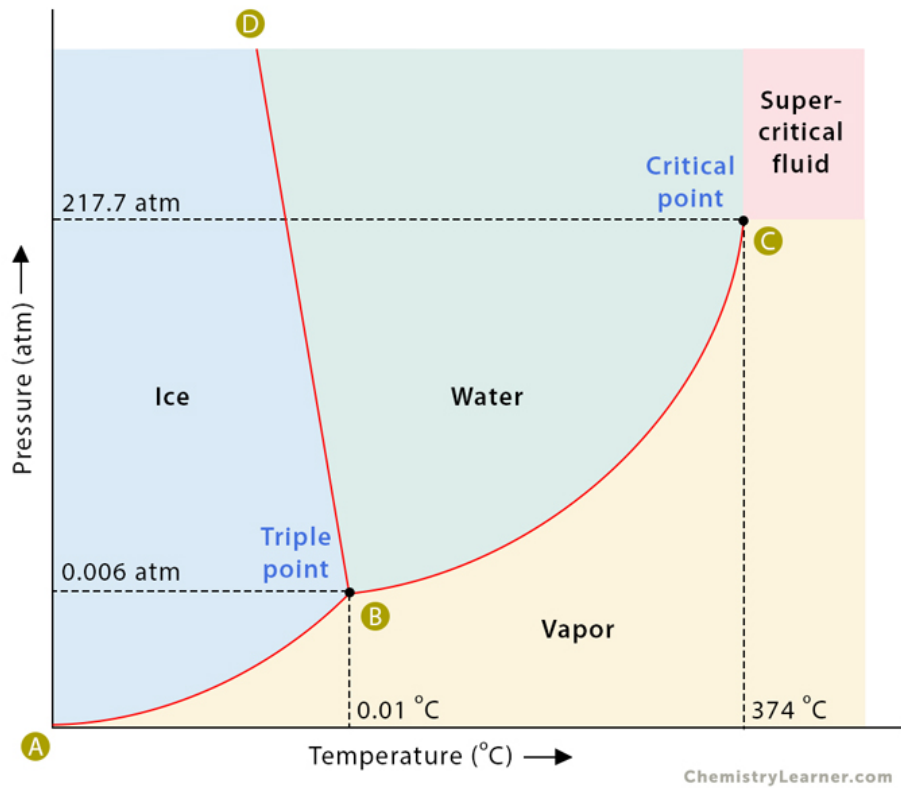
$$= -7.4957 \times 10^{-03} \text{ }^\circ\text{C atm}^{-1}$$

# Important Note

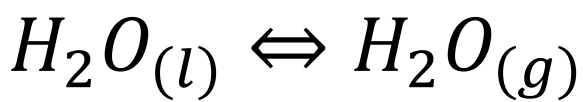
- ✚ Unlike all liquid/solid transformations, the mp of ice decreases with increasing P. Comment?
- ✚ Water is actually an **abnormal compound** because of the strong H-bonding between water molecules that makes the **volume increases** abnormally upon **freezing**.
- ✚ Hence, the **freezing/melting** line **in** water phase diagram has a negative slope.

$$\frac{dT}{dP} = -7.4957 \times 10^{-03} \text{ } ^\circ\text{C atm}^{-1}$$

# Phase Diagram of Water



# Water/vapor equilibrium



$$\Delta H_v = 40.66 \text{ kJ mol}^{-1} \text{ at } 373\text{K}$$

Eq.	$V_l$ $\text{cm}^3\text{mol}^{-1}$	$V_g$ $\text{cm}^3\text{mol}^{-1}$	$\Delta H$ , kJ $\text{mol}^{-1}$	$T_{eq}$ K
$H_2O_{(l)} \leftrightarrow H_2O_{(g)}$	<b>18.72</b>	<b>30078</b>	<b>40.66</b>	<b>373</b>

$$\Delta V = V_g - V_l \approx V_g = \frac{RT}{P} \rightarrow \frac{dP}{dT} = \frac{\Delta H}{T\Delta V} = \frac{P\Delta H}{RT^2}$$

$$\frac{dP}{P} = \frac{\Delta H}{R} \frac{dT}{T^2}$$

$$d \ln P = \frac{\Delta H_{vap}}{R} \frac{dT}{T^2}$$

$$\frac{d \ln P}{dT} = \frac{\Delta H_{vap}}{RT^2}$$

- ▶ If  $\Delta H_{\text{vap}}$  is known as a function of  $T$ , we can substitute easily. Otherwise, assume it independent of  $T$  over a limited small range of  $T$ .

$$\int d \ln P = \int \frac{\Delta H_{\text{vap}}}{R} \frac{dT}{T^2}$$

$$\ln P = \frac{-\Delta H_{\text{vap}}}{R} \frac{1}{T} + \text{const}$$

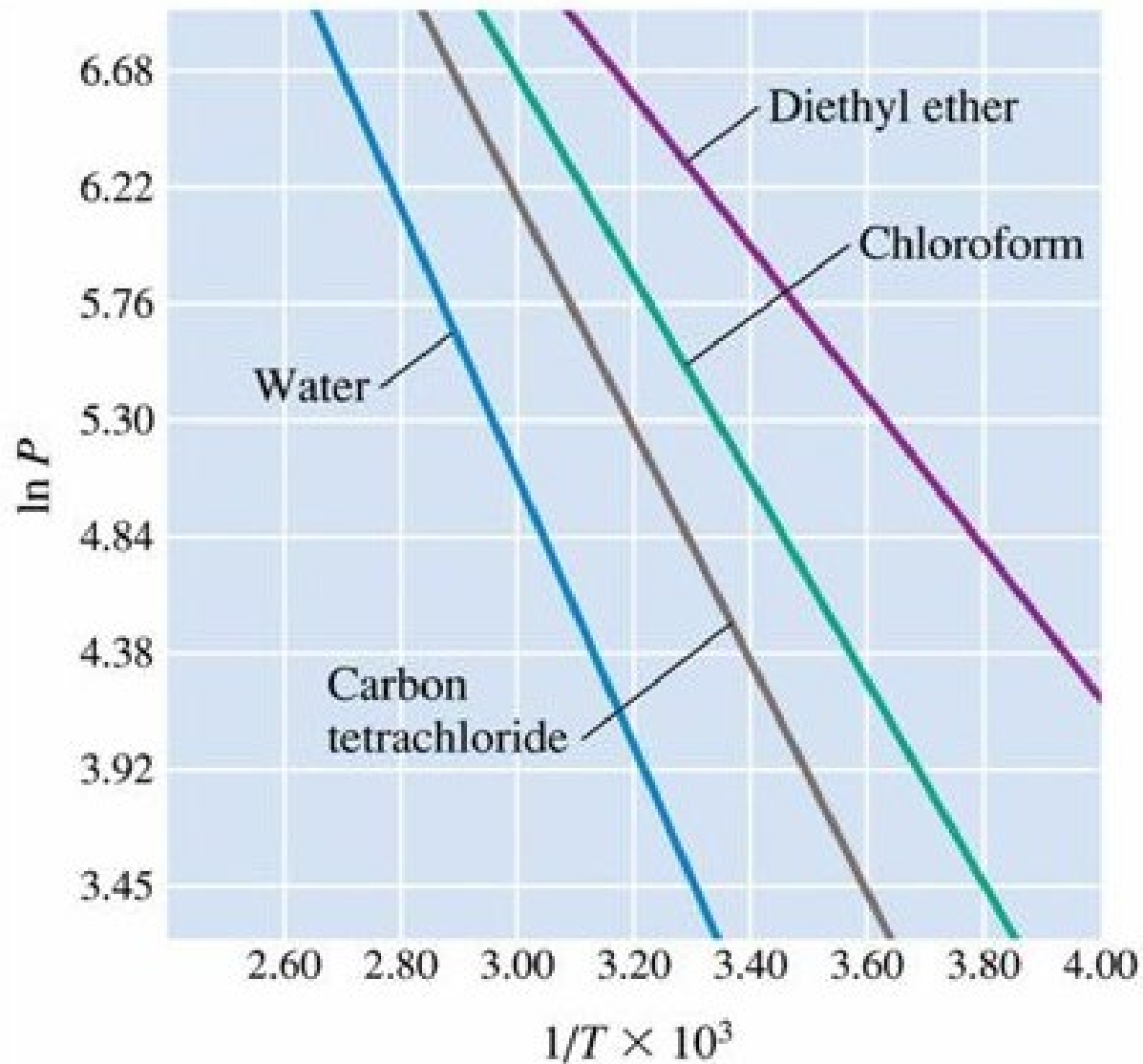
**ln P vs. 1/T is linear**

**P increases exponentially with T**

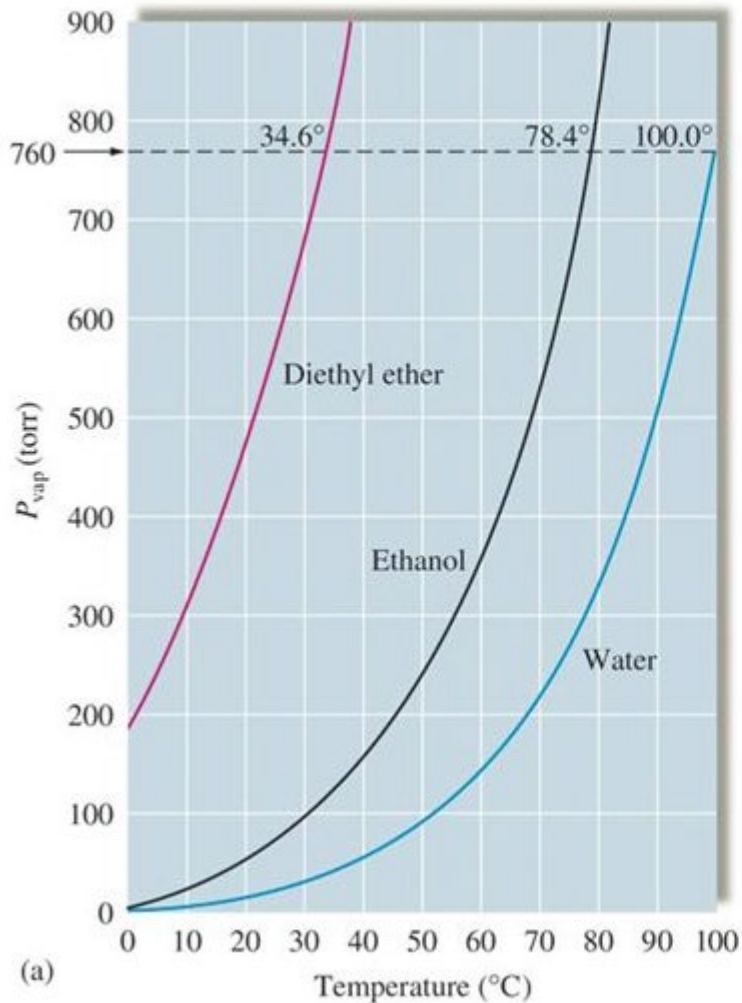
- As  $T \uparrow$ ,  $(1/T) \downarrow$ ,  $P \uparrow$  exponentially.
- It corresponds to variation of vapor pressure of liquids with  $T$

$$\ln P = \frac{-\Delta H_{vap}}{R} \frac{1}{T} + const$$

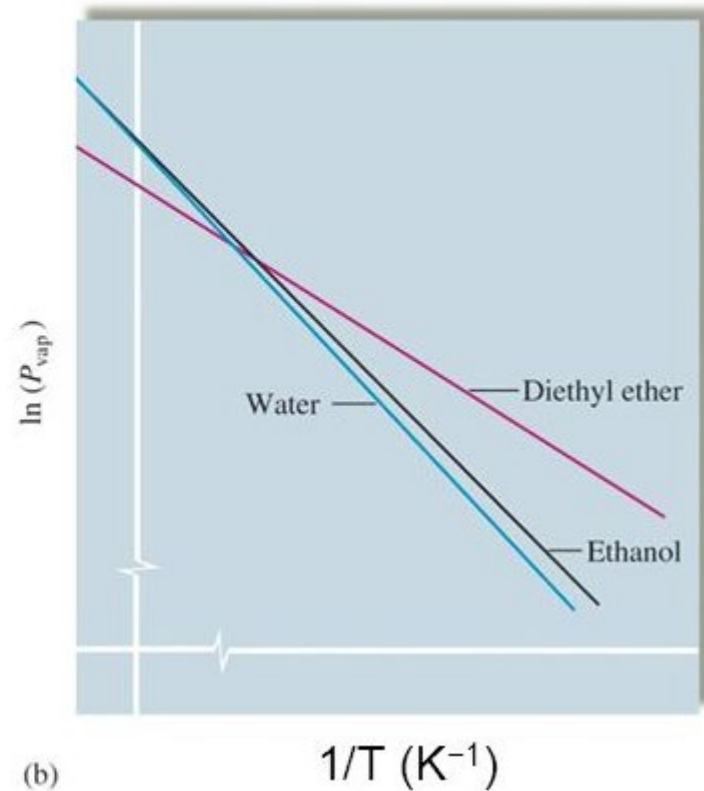
$$\ln \frac{P_2}{P_1} = \frac{\Delta H_{vap}}{R} \left( \frac{1}{T_1} - \frac{1}{T_2} \right)$$



$$\log \frac{P_2}{P_1} = \frac{\Delta H_{vap}}{2.303R} \left( \frac{1}{T_1} - \frac{1}{T_2} \right)$$



**T is in K!**



# Exercise

- ✚ The **standard** vapor pressure of benzene is **90.76** and **450.79** torr at **20** and **60** °C, respectively. Calculate:
- $\Delta H_{\text{vap}}$  for benzene?
  - the boiling point (bp) of benzene on a top of hill where the prevailing pressure is 622 torr?
  - the boiling point (bp) of benzene at the bottom of a valley where the prevailing pressure is 843 torr?

# Solution

$$\log \frac{P_2}{P_1} = \frac{\Delta H_{\text{vap}}}{2.303R} \left( \frac{1}{T_1} - \frac{1}{T_2} \right)$$

$$\log \frac{450.79}{90.76} = \frac{\Delta H_{vap}}{2.303(8.314 \text{ J K}^{-1} \text{ mol}^{-1})} \left( \frac{1}{293} - \frac{1}{333} \right)$$

$$\Delta H_{vap} = 32509.841 \text{ J mol}^{-1} = 32.5 \text{ kJ mol}^{-1} = 7.8 \text{ kcal mol}^{-1}$$

$$\log \frac{622}{90.76} = \frac{32509.841 \text{ J mol}^{-1}}{2.303(8.314 \text{ J K}^{-1} \text{ mol}^{-1})} \left( \frac{1}{293} - \frac{1}{T_2} \right)$$

$$T_2 = 438.7 \text{ K} = 165^\circ \text{ C}$$

$$\log \frac{843}{90.76} = \frac{32509.841 \text{ J mol}^{-1}}{2.303(8.314 \text{ J K}^{-1} \text{ mol}^{-1})} \left( \frac{1}{293} - \frac{1}{T_2} \right)$$

$$T_2 = 476.1 \text{ K} = 203^\circ \text{ C}$$

# Solid/Vapor (sublimation) equilibrium

- Many solids (e.g., iodine and dry ice (solid  $\text{CO}_2$ )) have measurable vapor pressure.
- The saturated vapor pressure of a certain solid is called the sublimation pressure, that can be obtained similarly as vapor pressure of liquids from Clapeyron's equation.

$$\ln P = \frac{-\Delta H_{sub}}{R} \frac{1}{T} + const$$

$$\ln \frac{P_2}{P_1} = \frac{\Delta H_{sub}}{R} \left( \frac{1}{T_1} - \frac{1}{T_2} \right)$$

$$\Delta H_{sub} = \Delta H_{fus} + \Delta H_{vap}$$

# Trouton's rule

- Over narrow ranges of  $T$ ,  $\Delta H_{\text{vap}}$  can be considered as a **linear** function of  $T$ .
- Over a wide range of  $T$ ,  $\Delta H_{\text{vap}}$  approaches zero at the **critical  $T$** , the temperature above which a gas cannot be **liquefied**, regardless of the pressure applied.
- If  $\Delta H_{\text{vap}}$  is not known, **Trouton's rule** estimates its value.
- Trouton's rule** states that the **entropy of vaporization** is almost the same value,  $\sim 85\text{--}88 \text{ J K}^{-1} \text{ mol}^{-1}$ , for various kinds of liquids at their standard (**1 atm**) boiling points.
- The **entropy of vaporization** is defined as the ratio between the *enthalpy of vaporization* and the **boiling temperature**.

$$\Delta S_{vap} = \frac{\Delta H_{vap}}{T_b} \cong 88 \text{ J K}^{-1} \text{ mol}^{-1}$$

## Richard's rule

✚ The **entropy of fusion** at the standard (1 atm) freezing point of a solid is constant, about **8.36 J K<sup>-1</sup> mol<sup>-1</sup>**.

$$\Delta S_{fus} = \frac{\Delta H_{fus}}{T_f} \cong 8.36 \text{ J K}^{-1} \text{ mol}^{-1}$$

# $\Delta G$ / activity relations

Consider this  
reaction



$G$  is related to the activity ( $a$ , effective concentration) of each species by:

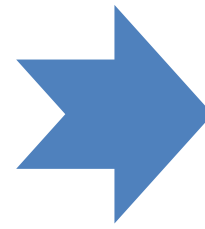
$$G_i = G_i^0 + RT \ln a_i$$

$G_i^0$  is the standard free energy at unit activity.

$$\Delta G = (cG_C + dG_D + \dots) - (aG_A + bG_B + \dots)$$

$$\Delta G = \Delta G^0 + RT \ln \frac{a_C^c a_D^d}{a_A^a a_B^b}$$

# Interpretation



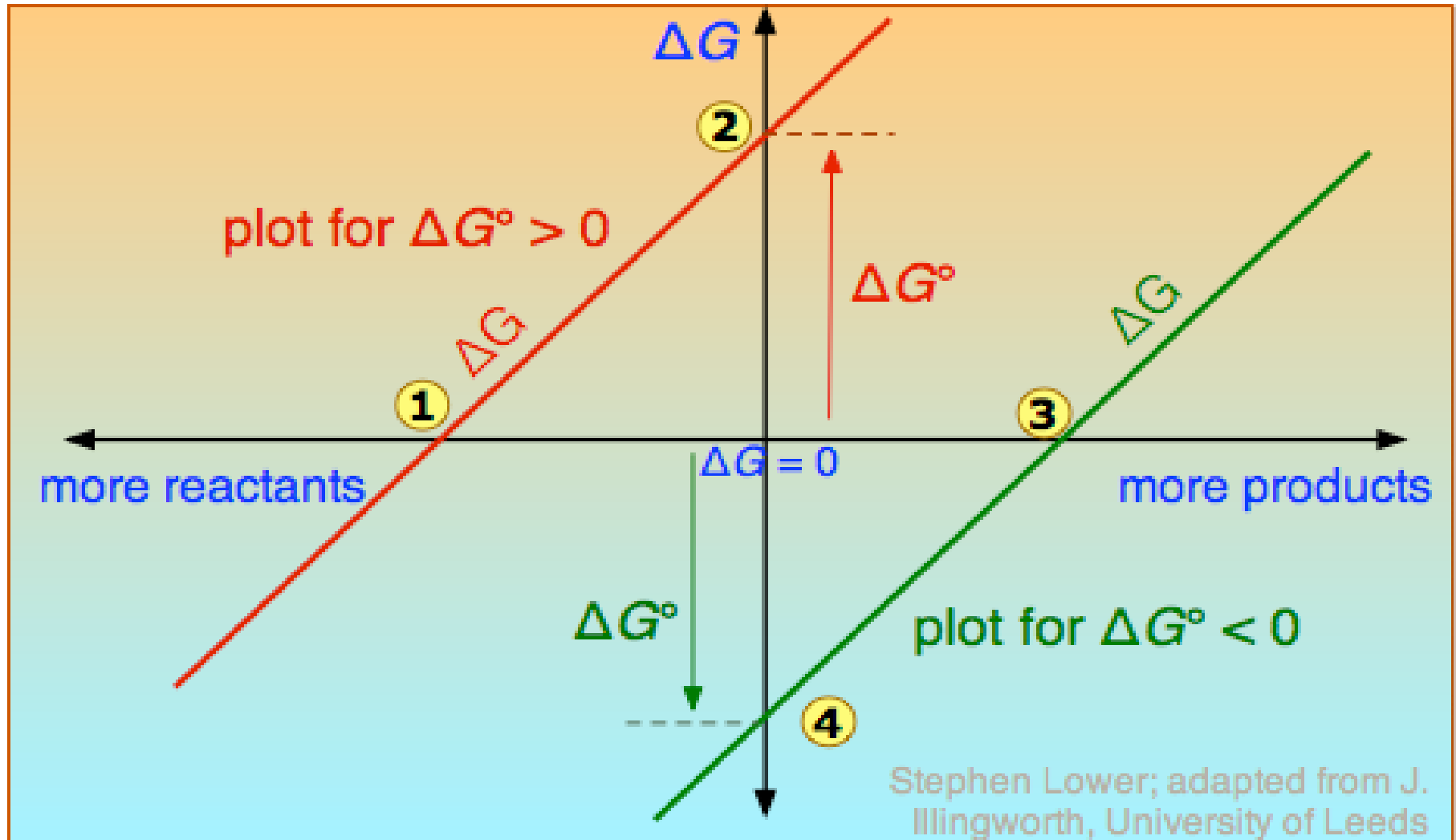
$$\Delta G = \Delta G^0 + RT \ln \frac{a_C^c a_D^d}{a_A^a a_B^b}$$

- As the reaction proceeds, the **activities** of products **increases** and those of reactants decreases; making  $\Delta G$  getting closer to zero (**equilibrium position**).
- Notice that before reaction,  $\Delta G$  was negative to drive the spontaneity.

# $\Delta G$ , $\Delta G_f^\circ$ , $\Delta G^\circ$

- $\Delta G^\circ$ : free energy change of a reaction when all components (reactants and products) are in their **standard states**.
- $\Delta G_f^\circ$ : free energy change of a reaction in which a substance is formed from the elements as they exist in their most stable forms at 1 atm pressure and (usually) 298 K.
- $\Delta G_f^\circ$  and  $\Delta H_f^\circ$  are by definition zero for elements in their **standard** states with some minor exceptions for  $\Delta G_f^\circ$ .
- $\Delta G$  is plotted on a vertical axis for two hypothetical reactions having opposite signs of  $\Delta G^\circ$ . The horizontal axis schematically expresses the **relative concentrations** of reactants and products at any point of the process.

# $\Delta G, \Delta G^{\circ}$



The **origin** corresponds to the composition at which half of the reactants have been converted into products

# *Important Remarks*

- ✚ For the red line ( $\Delta G^\circ > 0$ ) at (point 2)  $\Delta G = \Delta G^\circ$ .
- ✚ At point 1,  $\Delta G = 0$ ; some products have been formed, but the composition is still dominated by reactants.
- ✚ If we begin at a composition to the left of point 1,  $\Delta G$  will be negative and the composition will move to the right.
- ✚ Similarly, if we begin with a composition to the right of point 1,  $\Delta G$  will be positive and the composition will move to the left.

# Important Remarks

- ✚ For the green line ( $\Delta G^\circ < 0$ ),  $\Delta G^\circ$  is shown at **point 4**.
- ✚ At its equilibrium point (**point 3**,  $\Delta G = 0$ ), there are more products than reactants.
- ✚ If we start at a composition to the right of **point 3**, the composition will tend to move to the left. If the initial composition is to the left of **point 3**, the reaction will tend to proceed to the right.
- ✚ What would happen if  $\Delta G^\circ$  were 0? The equilibrium point of such a reaction would be at the origin, corresponding to half the reactants being converted to product.

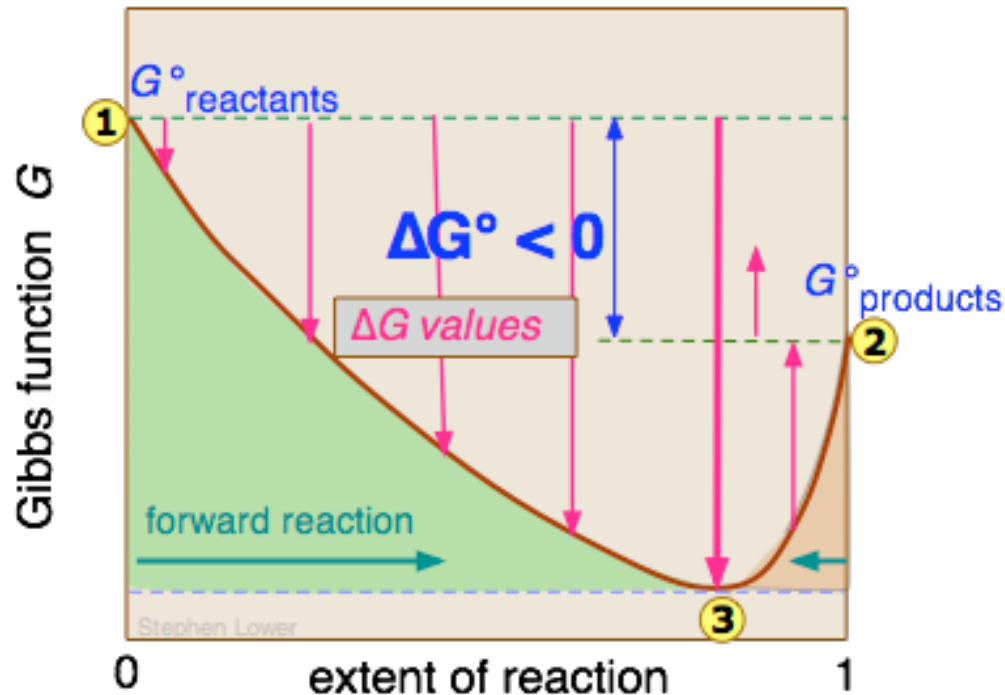
# *Important Principles*

- ✚ A **negative  $\Delta G^\circ$**  does not mean that the reactants will be completely transformed into products.
- ✚ By the same token, a **positive  $\Delta G^\circ$**  does not mean that no products are formed at all.
- ✚ The reason for the **Gibbs energy minimum** at **equilibrium** relates to the increase in entropy when products and reactants coexist in the same phase.

$$\Delta G^0 = \Delta H^0 - T\Delta S^0$$

# Spontaneous reactions

- Rx will take place spontaneously.
- This does not mean that each mole of pure A will be converted into one mole of pure B.

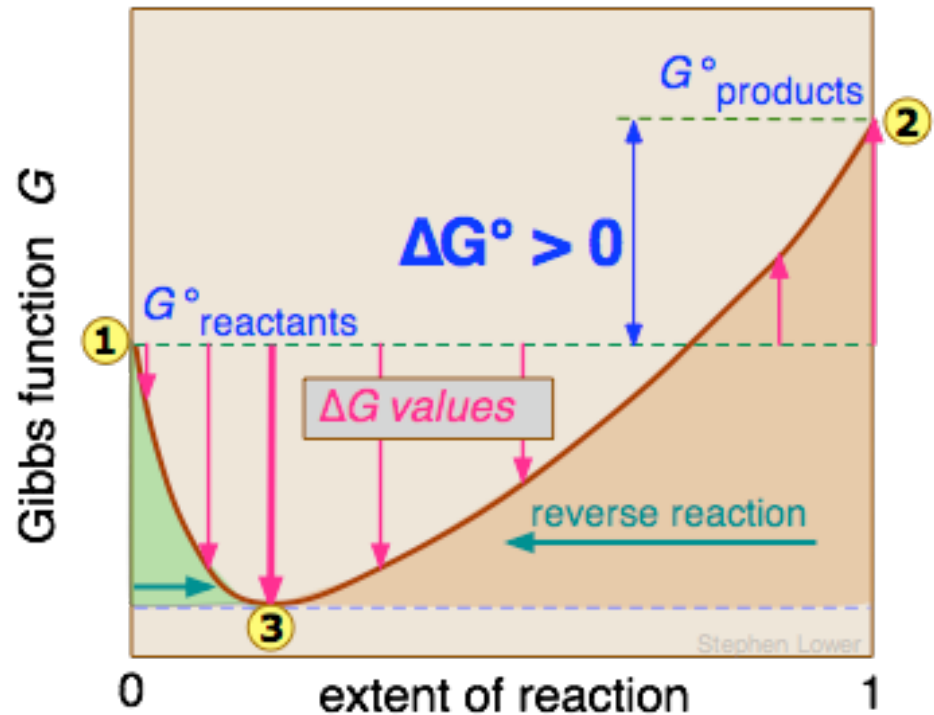


$$G^\circ(\text{reactants}) > G^\circ(\text{reactants})$$

- For reactions in which products and reactants occupy a single phase (gas or solution), the meaning of "spontaneous" is that the equilibrium composition will correspond to an extent of reaction greater than 0.5 but smaller than unity.

# Non-spontaneous reactions

- Rx will take place **non-spontaneously**.
- The equilibrium composition will correspond to an extent of reaction greater than zero but less than 0.5.



$$G^\circ (\text{reactants}) < G^\circ (\text{reactants})$$

- In this case, the minimum at **point 3** reflects the increase in entropy when the reactants are "**contaminated**" by a small quantity of products.

# Important Remarks

- ✚ For  $\Delta G^\circ > \pm 50 \text{ kJ mol}^{-1}$ , the equilibrium composition will be negligibly different from zero or unity extent-of-reaction.
- ✚ The **physical meaning of  $\Delta G$**  is that it tells us how far the free energy of the system has changed from  $G^\circ$  of the pure reactants (**point 1**).
- ✚ As the reaction proceeds to the right, the composition changes, and  $\Delta G$  begins to fall. When the composition reaches **point 3**,  $\Delta G$  reaches its minimum value and further reaction would cause it to **rise**.
- ✚ But because *free energy can only decrease* but never increase, this does not happen. The composition of the system remains permanently at its equilibrium value.

# $\Delta G$ / equilibrium constants

For this  
reaction



$$\Delta G = \Delta G^0 + RT \ln \frac{a_C^c a_D^d}{a_A^a a_B^b}$$

At equilibrium,  $\Delta G=0$

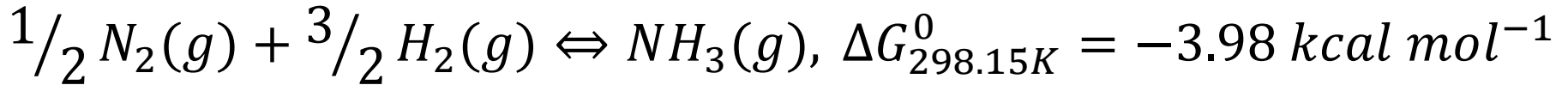
$$\Delta G^0 = -RT \ln \left( \frac{a_C^c a_D^d}{a_A^a a_B^b} \right)_{eq} = -RT \ln K_{th}$$

$K_{th}$  is called the thermodynamic  
equilibrium constant

$$K_{th} = \exp \left( \frac{-\Delta G^0}{RT} \right)$$

# Exercise

✚ Calculate the thermodynamic equilibrium constant for the following reaction:

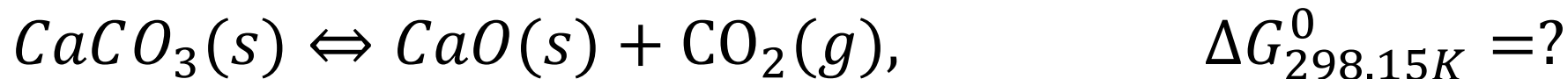


# Solution

$$K_{th} = \exp \left( \frac{-(-3980 \text{ cal mol}^{-1})}{(1.987 \text{ cal K}^{-1} \text{ mol}^{-1})(298.15 \text{ K})} \right) \\ = 827.1$$

# Exercise

Find the standard Gibbs energy change for the following reaction knowing these  $\Delta G^\circ$  for  $\text{CaCO}_3(s)$ :  $-1128 \text{ kJ mol}^{-1}$ ,  $\text{CaO}(s)$ :  $-603.5 \text{ kJ mol}^{-1}$ ,  $\text{CO}_2(g)$ :  $-137.2 \text{ kJ mol}^{-1}$ ?



# Solution

$$\begin{aligned} \Delta G^0 &= [(-603.5 - 137.2) - (-1128)] \\ &= +130.9 \text{ kJ mol}^{-1} \end{aligned}$$

**Process is not spontaneous** under standard conditions. If conditions are changed, this process can be spontaneous.

# Equilibrium /Conventional constants



$$K_{th} = \left( \frac{a_C^c a_D^d}{a_A^a a_B^b} \right)_{eq}$$

$$K = \frac{[C]^c [D]^d}{[A]^a [B]^b}$$

[ ] = molar concentration

$$a_A = \gamma_A [A]$$

$\gamma_A$ : activity coefficient of A

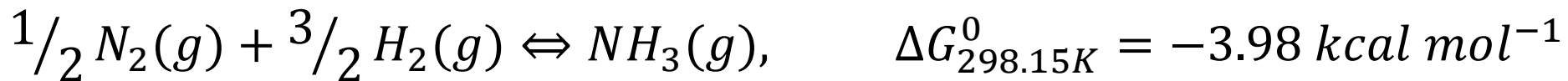
If  $\gamma_A = 1$ ,  $K = K_{th}$  for ideal dilute solutions

$$K_{th} = \left( \frac{a_C^c a_D^d}{a_A^a a_B^b} \right)_{eq} = K \left( \frac{\gamma_C^c \gamma_D^d}{\gamma_A^a \gamma_B^b} \right) = K K_\gamma$$

## Fugacity, $f$ (Effective pressure)

- Similar to activity and activity coefficient in solids and liquids, fugacity ( $f$ ) and fugacity coefficient  $\gamma$ , account for real gas corrected P.
- $\gamma = 1$  for ideal gases.

$$f = \gamma P$$



$$K_{th} = \frac{f_{NH_3}}{f_{N_2}^{1/2} f_{H_2}^{3/2}} = \left( \frac{P_{NH_3}}{P_{N_2}^{1/2} P_{H_2}^{3/2}} \right) \left( \frac{\gamma_{NH_3}}{\gamma_{N_2}^{1/2} \gamma_{H_2}^{3/2}} \right) = K_P K_\gamma$$

# Properties of $K$

- +  $K$  has a single constant value at a given temperature.
- + If  $T$  changes,  $\Delta H$  or better say  $\Delta G$  will change, hence  $K$ .
- +  $K$  is independent on the activity of reactants and products but for single  $K$  value at a given  $T$ , there are many equilibrium positions with different activities.
- + If a reaction is reversed, the new  $K$  will equal the reciprocal of the first one.

# Effect of T on K

$$\Delta G^0 = -RT \ln K$$

$$R \ln K = \frac{-\Delta G^0}{T} = \frac{-(\sum G_{products}^0 - \sum G_{reactants}^0)}{T}$$

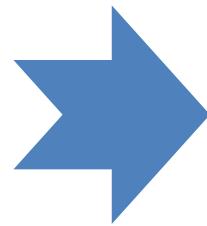
Differentiate  
with respect to T

$$\frac{d(R \ln K)}{dT} = \frac{-d(\Delta G^0/T)}{dT}$$

Previously we estimated

$$\frac{d(\Delta G/T)_P}{dT} = \frac{-\Delta H}{T^2}$$

# Interpretation



$$\frac{d(\ln K)}{dT} = \frac{\Delta H^0}{RT^2}$$

- ✚ This equation gives a quantification for **Le Chatelier's** principle in one of its aspects.
- ✚ For **exothermic** reactions,  $\Delta H^0 < 0$ , as  $T$  increases,  $K$  decreases. This means that increasing  $T$  favors the direction **to** the **reactants** and Vice versa.

$$\int d \ln K = \int \frac{\Delta H^0}{RT^2} dT$$

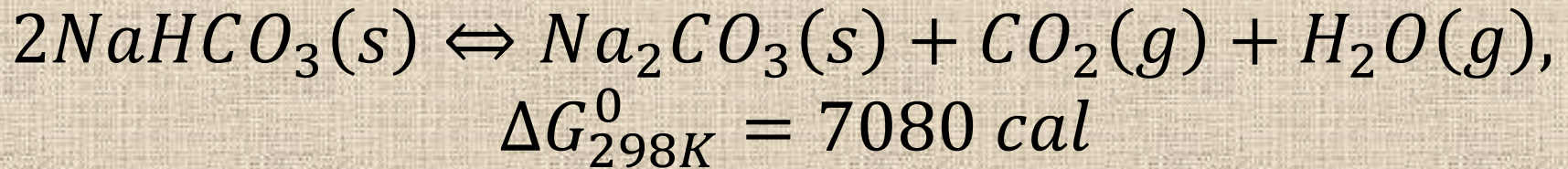
If  $\Delta H^0$  is independent of  $T$ ,  
(otherwise integrate it)

$$\ln K = \frac{-\Delta H^0}{RT} + \text{const}$$

$$\ln \frac{K_2}{K_1} = \frac{-\Delta H^0}{R} \left( \frac{1}{T_2} - \frac{1}{T_1} \right)$$

## Exercise

✚ Calculate the equilibrium constant at 250 K for the following reaction,



$$\Delta H^0 = 29320 + 9.15T - 12.75 \times 10^{-3}T^2$$

## Solution

$$\Delta G^0 = -RT \ln K$$

$$K = \exp\left(\frac{-\Delta G^0}{RT}\right) =$$

$$\exp\left(\frac{-7080 \text{ cal}/2\text{mol}}{(1.987 \text{ cal K}^{-1} \text{ mol}^{-1})(298 \text{ K})}\right) = 394.83$$

$$\frac{d(\ln K)}{dT} = \frac{\Delta H^0}{RT^2}$$

$$\int d \ln K$$

$$= \int \frac{(29320 + 9.15T - 12.75 \times 10^{-3}T^2)}{RT^2} dT$$

$$\ln \frac{K_2}{K_1} = \frac{\left( \left( \frac{-29320}{T_2 - T_1} \right) + 9.15 \ln \frac{T_2}{T_1} - 12.75 \times 10^{-3} (T_2 - T_1) \right)}{R}$$

$$\ln \frac{K_2}{394.83} = \frac{\left( \left( \frac{-29320}{250 - 298} \right) + 9.15 \ln \frac{250}{298} - 12.75 \times 10^{-3} (250 - 298) \right)}{1.987 \text{ cal } K^{-1} \text{ mol}^{-1}}$$

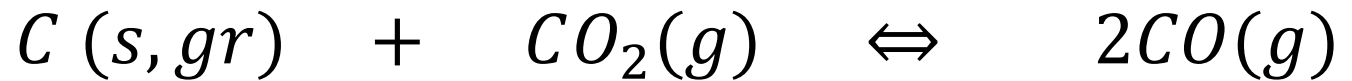
# Effect of P on K

- ✚ The extent of a reaction means the degree or percentage to which the reactants have changed to products.
- ✚ The extent of reaction depends on  $P$  (for gases) or concentration ( $C$ ) and temperature.
- ✚ The effect of  $P$  or  $C$  on the extent of reaction depends on the nature of reactions, i.e., no of moles of gaseous reactants and products and activity coefficients.

# Exercise

Find the effect of pressure on the Boundouard's reaction?

# Solution



Start with 1 mol

$1-\alpha$

$2\alpha$

Total moles at eq. =  $1+\alpha$

Start with n mol

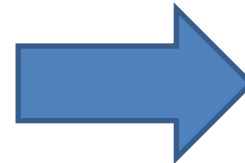
$n(1-\alpha)$

$2n\alpha$

Total moles at eq. =  $n(1+\alpha)$

$$K_{th} = \left( \frac{P_{CO(g)}^2}{P_{CO_2(g)}} \right) \left( \frac{\gamma_{CO(g)}^2}{\gamma_{CO_2(g)}} \right)$$

Ideal  
behavior



$$K_{th} = \left( \frac{P_{CO(g)}^2}{P_{CO_2(g)}} \right)$$

Partial pressures can be calculated from **Dalton's** law

$$P_i = X_i P_t$$

Start with 1 mol CO<sub>2</sub>

$$P_{CO_2} = X_{CO_2} P_t = \left( \frac{1 - \alpha}{1 + \alpha} \right) P_t$$

$$P_{CO} = X_{CO} P_t = \left( \frac{2\alpha}{1 + \alpha} \right) P_t$$

Ideal behavior

$$K_{th} = \left( \frac{P_{CO(g)}^2}{P_{CO_2(g)}} \right) = \left( \frac{\left( \left( \frac{2\alpha}{1 + \alpha} \right) P_t \right)^2}{\left( \frac{1 - \alpha}{1 + \alpha} \right) P_t} \right)$$

$$= \frac{4\alpha^2 P_t}{(1 + \alpha)(1 - \alpha)} = \frac{4\alpha^2 P_t}{1 - \alpha^2}$$

as  $P_t$  increases,  $\alpha$  increases in order to sustain a

**constant**  $K_{th}$

# Effect of inert gases on $\alpha$

- ✚ For ideal gas mixtures, where  $\gamma=1$ , adding **inert** (**non reacting**) gases to a chemical reaction does not affect  $K$ .
- ✚ For **non-ideal** gas mixtures, adding inert (**non reacting**) gases to a chemical reaction affect  $\gamma$  and hence  $\alpha$  to keep  $K$  constant

## For Boudouard's reaction

$$K_{th} = \left( \frac{P_{CO(g)}^2}{P_{CO_2(g)}} \right) \left( \frac{\gamma_{CO(g)}^2}{\gamma_{CO_2(g)}} \right) = \frac{4\alpha^2 P_t}{1 - \alpha^2} \left( \frac{\gamma_{CO(g)}^2}{\gamma_{CO_2(g)}} \right)$$

# Thermodynamics prediction

- ✚ The practical importance of the **Gibbs energy** is that it allows us to make **predictions** based on the properties ( **$\Delta G^\circ$  values**) of the reactants and products themselves, eliminating the need to experiment.
- ✚ While thermodynamics always correctly predicts whether a given process can take place (**spontaneous**), it is unable to tell us if it will take place at an **observable rate**.

When thermodynamics says "**no**", it means exactly ***that***.

When it says "**yes**", it means "***maybe***".

# Exercise

## H<sub>2</sub>/O<sub>2</sub> Fuel Cells

✚ The reaction  $\frac{1}{2} \text{O}_2 (\text{g}) + \text{H}_2 (\text{g}) \rightarrow \text{H}_2\text{O}(\text{l})$  is used in fuel cells to produce an electrical current. The reaction can also be carried out by direct combustion. Thermodynamic data: molar entropies in  $\text{J mol}^{-1} \text{K}^{-1}$ :  $\text{O}_2(\text{g})$  205.0;  $\text{H}_2(\text{g})$  130.6;  $\text{H}_2\text{O}(\text{l})$  70.0;  $\Delta H_f^\circ$  of  $\text{H}_2\text{O}(\text{l}) = -285.9 \text{ kJ mol}^{-1}$ . Use this information to find

- the amount of heat released when the reaction takes place by **direct combustion**;
- the amount of **electrical work** the same reaction can perform when carried out in a fuel cell at 298 K under reversible conditions;
- the amount of **heat released** under the same conditions.

# Solution

- ▶ First, we need to find  $\Delta H^\circ$  and  $\Delta S^\circ$  for the process.
- ▶ Recalling that the standard enthalpy of formation of the elements is zero,

$$\begin{aligned}\Delta H^0 &= \Delta H_f^0(\text{products}) - \Delta H_f^0(\text{reactants}) \\ &= -285.9 \text{ kJ mol}^{-1} - 0 = -285.9 \text{ kJ mol}^{-1}\end{aligned}$$

$$\begin{aligned}\Delta S^0 &= S_f^0(\text{products}) - S_f^0(\text{reactants}) \\ &= (70.0) - (\frac{1}{2} \times 205.0 + 130.6) \\ &= -163 \text{ J K}^{-1} \text{ mol}^{-1}\end{aligned}$$

a) When  $\text{H}_2$  and  $\text{O}_2$  are **combined directly**, the heat released will be  **$\Delta H^\circ = -285.9 \text{ kJ mol}^{-1}$** .

b) The **maximum electrical work** the fuel cell can perform is given by

$$\begin{aligned}\Delta G^0 &= \Delta H^0 - T\Delta S^0 = \\ (-285.9 \text{ kJ mol}^{-1}) &- [(298 \text{ K})(-163 \text{ JK}^{-1} \text{ mol}^{-1})] \\ &= -237.2 \text{ kJ mol}^{-1}\end{aligned}$$

c) The heat released in the fuel cell reaction is the difference between the enthalpy change (the total energy available) and the reversible work that was expended

$$\begin{aligned}\Delta H^0 - \Delta G^0 &= T\Delta S^0 = \\ [(298 \text{ K})(-163 \text{ JK}^{-1} \text{ mol}^{-1})] &= -48800 \text{ J mol}^{-1} \\ &= -48.8 \text{ kJ mol}^{-1} = -237.2 \text{ kJ mol}^{-1}\end{aligned}$$

# Note

- ✓ In this Rx 1.5 moles of gas disappear, to be replaced by 18 mL (1 mole) of water.
- ✓ The system undergoes a marked contraction in which the atmosphere performs pressure-volume work on the system.
- ✓ But this PV work is the "non-useful" work that is not included in the  $\Delta G$  value.

# Absolute Entropy

## Third Law of Thermodynamics

*The entropy of any **pure perfectly crystalline solid** is **ZERO** at the **absolute zero (0 K)**.*

### Criteria

- Pure:** because impure substances would have a finite entropy at 0K ( $\Delta S$  of mixing the substance with impurities)
- Perfectly:** because imperfections would add crystal defects that increase the disordering and  $S$
- Solid:** because liquids have a finite entropy even at 0K which equals  $\Delta S$  of fusion

# Absolute S of pure perfectly crystalline solids at a given T

$$\int_{S_0}^{S_T} dS = S_T - S_0 = \int_0^T \frac{C_P}{T} dT = \int_0^T C_P d \ln T$$

$$S_T = S_0 + \int_0^T C_P d \ln T$$

$$S_0 = 0 \text{ at } 0 \text{ K}$$

$$S_T = \int_0^T \frac{C_P}{T} dT$$

As  $C_P$  is always +Ve,  $S_T$  should also be +Ve

At very low temperatures,

$$C_P = aT^3$$

Debye's Law of third power

$$S_T = \int_0^T \frac{aT^3}{T} dT = \int_0^T aT^2 dT = \frac{aT^3}{3} = \frac{C_P}{3}$$

The **absolute entropy** of a certain pure crystalline solid at low temperature is **one third** of its **heat capacity**

End of Class



Your *Duaa*

